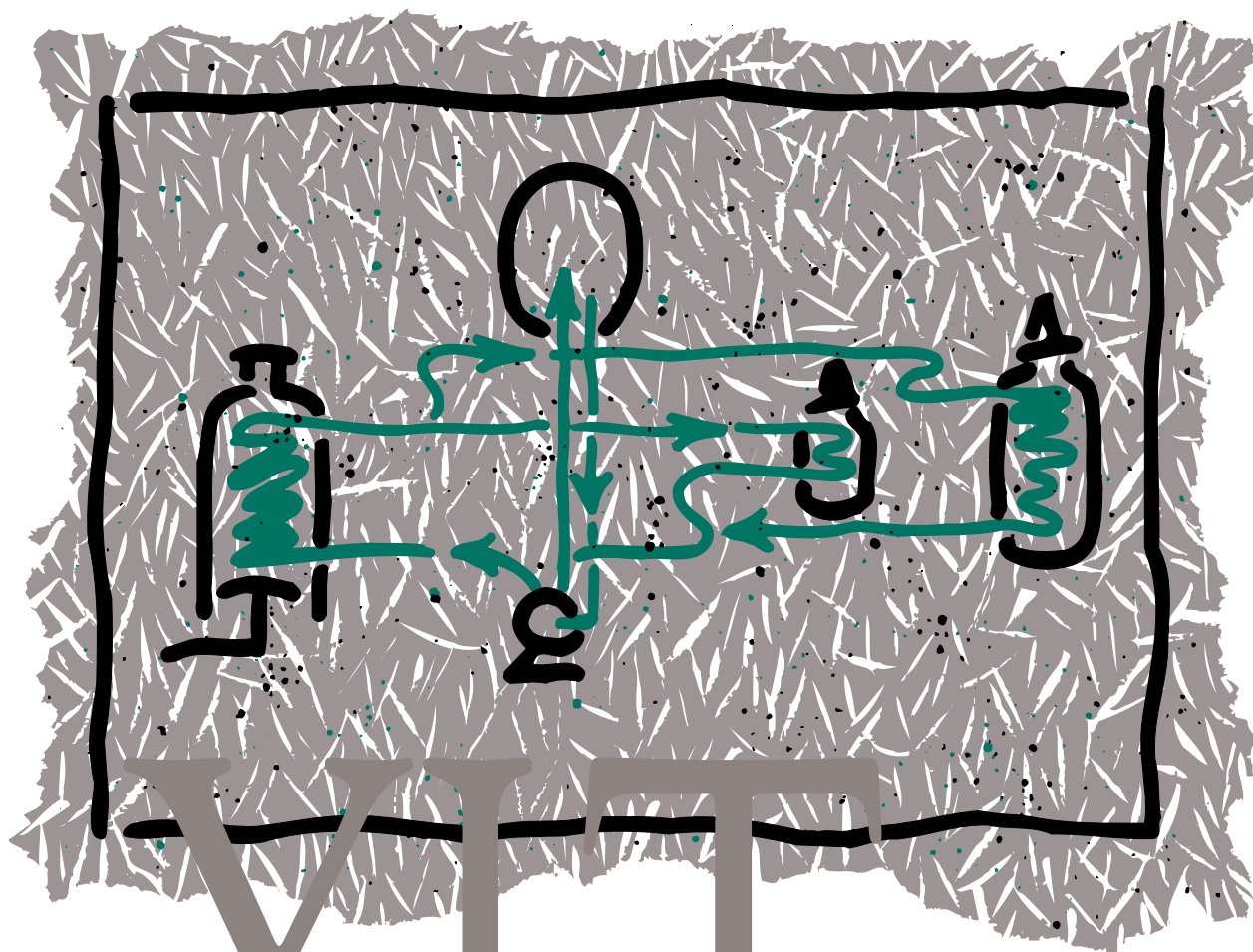




SYLTHERM XLT Heat Transfer Fluid



XLT

Product Technical Data

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SYLTHERM XLT HEAT TRANSFER FLUID

A Very Low Odor, Long-lasting Heat Transfer Fluid That's Ideal for Batch Processing

SYLTHERM XLT[†] heat transfer fluid is a specially formulated, high performance silicone polymer designed for use as a low temperature, liquid phase heat transfer medium. With a recommended use temperature range of -150°F to 500°F (-100°C to 260°C), SYLTHERM XLT fluid offers outstanding low temperature heat transfer and pumpability, plus excellent thermal stability. In addition, SYLTHERM XLT fluid has essentially no odor, is low in acute oral toxicity, and is not listed as reportable under SARA Title III, Section 313.¹ These features make SYLTHERM XLT fluid a viable alternative to many organic heat transfer fluids, chlorinated solvents, and CFCs that are presently used for low temperature, liquid phase service.

At -150°F, the viscosity of SYLTHERM XLT heat transfer fluid is only 90.2 centipoise (at -100°C the

viscosity is 78.6 mPa·s). A low viscosity at low operating temperatures is a critical property because it allows high heat transfer coefficients with low pressure drops and pumping horsepower.

The -150°F to 500°F (-100°C to 260°C) operating range of SYLTHERM XLT fluid makes it ideal for single fluid process heating and cooling applications (batch processing). Single fluid processing with SYLTHERM XLT fluid eliminates process interruption and the loss of temperature control associated with multiple fluid systems. Batch processing with SYLTHERM XLT fluid also eliminates system flush requirements associated with steam/brine and steam/glycol systems. SYLTHERM XLT fluid is noncorrosive toward metals and alloys commonly found in heat transfer systems.

In addition to the performance advantages of SYLTHERM XLT fluid, Dow's supporting services are unequalled. They include technical backup in the design phase, during operation, and after shutdown. Moreover, free analytical testing is provided to monitor fluid condition.

For Information About Our Full Line of Fluids...

To learn more about the full line of heat transfer fluids manufactured or distributed by Dow — including DOWTHERM* synthetic organic, SYLTHERM[†] silicone and DOWTHERM, DOWFROST*, and DOWCAL* glycol-based fluids — request our product line guide. Call the number for your area listed on the back of this brochure.

**Trademark of The Dow Chemical Company*

†Trademark of Dow Corning Corporation

¹You may need to comply with similar or additional legislation in other countries. Contact your Dow representative for information.

FLUID SELECTION CRITERIA

When evaluating thermal fluids for specific applications, a variety of characteristics should be considered. Four of the most important are thermal stability, human health and environmental regulatory status, freeze point, and viscosity.

Stability

SYLTHERM XLT fluid offers excellent thermal stability at temperatures between -150°F (-100°C) and 500°F (260°C). The maximum recommended film temperature is 550°F (290°C).

Within its recommended use range, SYLTHERM XLT heat transfer fluid will not degrade to form solids or volatile compounds having substantially higher vapor pressures. As a result, system downtime for periodic fluid reprocessing and replacement is eliminated. SYLTHERM XLT fluid can tolerate occasional high-temperature upsets with only minimal change to the physical properties of the fluid. However, extended use at bulk temperatures above 500°F (260°C) or film temperatures greater than 550°F (290°C), has the potential to generate higher system pressures and cause polymer cross-linking to occur. This will eventually cause the viscosity of the fluid to increase to a point where replacement will be required to restore system performance.

Low Odor, Non-reportable

SYLTHERM XLT fluid is virtually odorless and is low in acute oral toxicity. In addition, it is not listed as reportable under SARA Title III, Section 313.¹ SYLTHERM XLT fluid is well suited for use in pharmaceutical, fine chemical, and other processes where these properties are desired.

¹You may need to comply with similar or additional legislation in other countries. Contact your Dow representative for information.

SYLTHERM XLT fluid is composed primarily of volatile methylsiloxanes (VMS's). Until recently, VMS fluids were classified as volatile organic compounds (VOC's) by the EPA. Their status changed with the agency's ruling of Oct. 5, 1994, which declared VMS fluids to be exempt from that classification. The rule became final December 5, 1994. Basically, the EPA said that VMS fluids do not contribute to declining air quality; i.e., smog.

Freeze Point

SYLTHERM XLT fluid remains liquid below -150°F (-100°C). Freeze point is -168°F (-111°C). This eliminates many of the problems associated with cold weather start-ups and shutdowns. Steam or electrical tracing, which is costly to install and operate, is not needed.

Viscosity

The excellent viscosity characteristics of SYLTHERM XLT fluid at low temperatures make it an efficient choice for very low temperature applications. The low viscosity of SYLTHERM XLT fluid at low temperatures (only 90.2 cps at -150°F, 78.6 mPa·s at -100°C) minimizes pressure drop and reduces pumping horsepower requirements. In addition, high heat transfer coefficients can be obtained over the fluid's entire temperature range. This can reduce refrigeration equipment energy consumption and cut process heat exchanger surface area requirements.

Thermal Stability

The thermal stability of a heat transfer fluid is dependent not only on its chemical structure but also on the design and operating temperature profile of the system in which it is used. Maximum fluid life can be

obtained by following sound engineering practices in the design of the heat transfer system. Three key areas of focus are: designing and operating the heater and/or energy recovery unit, preventing chemical contamination, and eliminating contact of the fluid with air.

Heater Design and Operation

Poor design and/or operation of the fired heater can cause overheating, resulting in excessive thermal degradation of the fluid.

When heaters are operated at high temperatures, fluid velocity in fired heaters should be a minimum of 6 feet per second (2 m/s); a range of 6 to 12 feet per second (2 to 4 m/s) should cover most cases. The actual velocity selected will depend on an economic balance between the cost of circulation and heat transfer surface. Operating limitations are usually placed on heat flux by equipment manufacturers. This heat flux is determined for a maximum film temperature by the operating conditions of the particular unit. Some problem areas to be avoided include:

1. Flame impingement.
2. Operating the heater above its rated capacity.
3. Modifying the fuel-to-air mixing procedure to change the flame height and pattern. This can yield higher flame and gas temperatures together with higher heat flux.
4. Low fluid velocity/high heat flux areas resulting in excessive heat transfer fluid film temperatures.

The manufacturer of the fired heater should be the primary contact in supplying you with the proper equipment for your heat transfer system needs.

Contamination Effects

SYLTHERM XLT heat transfer fluid is not sensitive to contamination by common piping contaminants, including water (during start-up and dry-out operations), rust, mill scale, lubricants, pipe dope, and small amounts of solvent and organic heat transfer fluid residue. SYLTHERM XLT fluid is somewhat more sensitive to contamination by acids or bases at elevated temperatures. As a result, lower molecular weight cyclic siloxanes can form and can raise the freeze point of the fluid. Similarly, contamination by water, oxygen, or other oxidants when the fluid is at an elevated temperature can result in cross-linking of polymer molecules and, if not corrected, can cause a gradual increase in viscosity. In order to minimize the likelihood of oxygen contamination, the system expansion tank should have an inert gas (such as nitrogen) blanket.

Expansion Tank

Figure 1 (page 7) is a simplified schematic of a recommended system loop design for SYLTHERM XLT heat transfer fluid. The expansion tank is positioned at the highest point in the system and has the capability for full flow of the heat transfer fluid through the tank. This design allows the expansion tank to be the lowest pressure point in the system, and the constant flow of heat transfer fluid through the tank ensures that vapors form only in the expansion tank. Once the system is heated up to the appropriate temperature and operating normally, system pressure will slowly increase until either the pressure in the expansion tank reaches the setting on the back

pressure regulator valve, or the system reaches the vapor pressure for the temperature of the fluid in the expansion tank. When the back pressure regulator is set at a pressure lower than the equilibrium vapor pressure of the fluid for a given temperature, periodic venting of the volatile materials will take place. The fluid will suffer no deleterious effect; however, periodic additions of fluid will be needed to maintain system volume.

An inert gas (such as nitrogen) blanket on the expansion tank is required to prevent the fluid from coming into contact with the outside air. Without this inert gas blanket, humid, outside air is likely to be drawn into the tank whenever the system cools below its normal operating temperature. This moisture contamination can result in increased pressure in the system due to steam formation on the next heat-up cycle or form ice in refrigeration equipment during low temperature operation. To avoid this, the inert gas supply regulator should be adjusted and maintained at a low setting (3–5 psig, 0.2–0.4 bar). This will minimize both the inert gas consumption and the additive effects of the blanket gas on total system pressure.

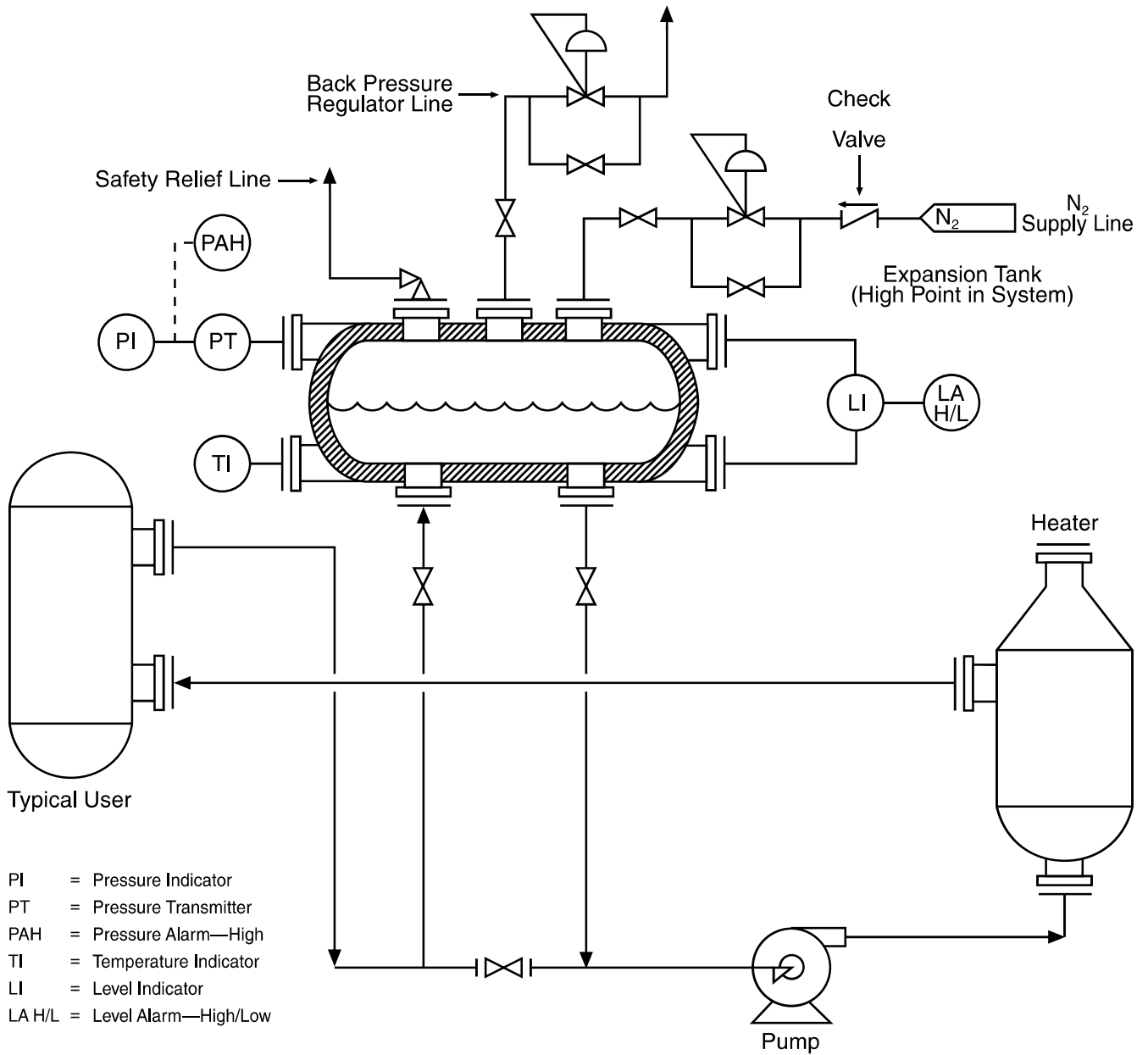
To prevent pump cavitation, the fluid pressure at the entrance to the pump must be above its vapor pressure, and there must be sufficient head in addition to the vapor pressure to satisfy the Net Positive Suction Head (NPSH) requirements of the pump. If the expansion tank is designed as shown in Figure 1, the back pressure regulator setting on the expansion tank will control the pressure at the entrance to the pump. The regulator set point should be 10 to 15 psi (0.7 to 1 bar) above the vapor pressure corresponding to the fluid temperature in the expansion tank.

NPSH requirements are primarily satisfied by the elevation of the expansion tank. The elevation is determined by calculating the total head necessary to overcome frictional line losses and specific NPSH requirements of the pump. In systems where such tank elevation is not practical, NPSH requirements can be met by increasing the amount of the blanket gas (usually nitrogen) in the vapor space of the expansion tank, thereby increasing the overall pressure in the tank. However, the additional system pressure created by the nitrogen should be accounted for during the system design.

The expansion tank design must satisfy two necessary requirements for proper start-up and operation of the system. First, the system piping to the expansion tank should be designed to permit full flow of fluid through the tank. A double drop leg design (see Figure 1) is the most effective arrangement to remove air, water vapors, and other noncondensibles during system start-up. For on-going operation, flow of fluid through the tank can often be reduced as long as sufficient flow is maintained to prevent pump cavitation. The tank and connecting piping should also be insulated to prevent the condensation of any vapors that may accumulate in this portion of the system.

Second, the inert gas blanket on the expansion tank should allow for a continuous flow of inert gas to be purged through the vapor space during the initial start-up. Separate inert gas supply and discharge nozzles, spaced as far apart as possible, will help ensure that any volatile contaminants (such as water or solvents) will be swept from the system during initial start-up.

Figure 1—Simplified System Schematic for SYLTHERM XLT Heat Transfer Fluid



The vent lines from the safety relief valve and back pressure regulator should be discharged to a safe area away from open flame and other potential sources of ignition. An appropriate outside container located well away from building air-intake fans is recommended. The vented volatile materials will be typically classified as flammable.

The expansion tank should be sized so that it is approximately 1/4 full when the system is at ambient temperature, and 3/4 full when the system is at its maximum operating temperature. Expansion tank instrumentation and fittings must meet the design requirements of the anticipated operating temperatures and pressures of the system and should include (refer to Figure 1):

1. Electronic level gauge covering the full fluid level range.
2. Fluid temperature indicator.
3. Level alarm (high/low) with low level shutdown to protect pump.
4. Pressure indicator with high pressure alarm.

Corrosivity

SYLTHERM XLT heat transfer fluid is noncorrosive toward common metals and alloys used in heat transfer systems, as long as it remains uncontaminated. Even at the high temperatures involved, equipment usually exhibits excellent service life.

Carbon steel is used predominantly in heat transfer systems utilizing SYLTHERM XLT fluid, although low

alloy steels, stainless steels, monel alloys, etc., are also used in miscellaneous pieces of equipment and instruments.

Most corrosion problems are caused by chemicals introduced into the system during cleaning or from process leaks. The severity and nature of the corrosivity will depend upon the amounts and type of contamination involved.

When special materials of construction are used, extra precaution should be taken to avoid contaminating materials containing the following:

Construction Material	Contaminant
<i>Austenitic Stainless Steel</i>	<i>Chlorides</i>
<i>Nickel</i>	<i>Sulfur</i>
<i>Copper Alloys</i>	<i>Ammonia</i>

Flammability and Fire Hazards

SYLTHERM XLT heat transfer fluid is a combustible material with a flash point of 116°F (47°C), a fire point of 130°F (54°C) C.O.C., and an autoignition temperature of 662°F (350°C) ASTM Method D-2155.

Vapor leaks to the atmosphere are sometimes encountered. Such leaks, however small, should not be tolerated because of the cost of replacing lost medium. Experience has shown that leaking vapors have usually cooled well below the fire point, and fire has rarely resulted.

Leaks from flanges or valves into insulation are also potentially hazardous because they can lead to fires in the insulation. It has been found, for example, that leakage of organic

materials into some types of insulation at elevated temperatures may result in spontaneous ignition due to auto-oxidation.

Vapors of SYLTHERM XLT fluid do not pose a serious flammability hazard at room temperature because the saturation concentration is so far below the lower flammability limit that ignition is extremely unlikely. Flammable mists are, however, possible under unusual circumstances where the time of exposure to an ignition source, the temperature of the source and the atmosphere, the volume of mixture, the fuel-air ratio, and the mist particle size all fall within a somewhat narrow range.

Static Spark Hazard

Heat transfer fluids like SYLTHERM XLT heat transfer fluid are generally poor electrical conductors, which means they can build up static charges and discharge static electricity within vessels or while being drained out of vessels. Therefore, safe engineering practice dictates that oxygen must be excluded from the headspace of the expansion tank. Similar precautions concerning static sparks should be taken when loading and unloading used fluid and volatiles.

Flammable-gas Detectors

Silicone vapors can deactivate many brands of flammable-gas detectors. However, several manufacturers offer detectors for silicone environments and report the operating life of these detectors is not affected by the presence of silicone materials. Contact your Dow Technical Service representative at the number for your area listed on the back of this brochure for listings of suppliers of these detectors.

NEW SYSTEM START-UP

The following information is a brief summary of the general recommendations and procedures for starting up a system with SYLTHERM XLT heat transfer fluid.

Prior to start-up, the system must be cleaned of dirt, welding slag, and other miscellaneous debris. Extra care taken to keep the system clean during construction can eliminate extensive cleaning prior to start-up. As mentioned previously, it is also very important to remove any residual water from the system prior to the installation of SYLTHERM XLT heat transfer fluid.

Because the design of all heat transfer systems differs to some extent, a detailed set of start-up procedures covering all possible systems is not practical. Users should develop procedures based on their own internal standards and recommendations from heat transfer equipment suppliers. The following procedures are presented as general guidelines only.

1. If the system is flushed with water or a suitable solvent, be sure that the fluid is circulated sufficiently through the system to pick up any remaining oils and debris. The pump and suction strainer should be checked periodically during this time to ensure that any collected debris is not severely restricting fluid flow to the pump inlet. If a filter is installed, filter the fluid for as long as practical through a 10-micron filter.

2. Completely drain the flush fluid by pressurizing the system with nitrogen or dry air, and opening all low-point drains. Alternately open and close all drain valves to increase the velocity of the gas flow. This will help to remove residual water/solvent and loose foreign particles.
3. Fill the system with SYLTHERM XLT heat transfer fluid. Circulate the fluid cold. Check for and repair any leaks. If a flush fluid was not used, check the pump suction strainers for any collected solids. If a filter is installed, continue circulating the fluid through the filter until the upper temperature limit of the filter is approached.
4. For the initial stages of start-up, the inert gas blanket system on the expansion tank should be arranged to allow a steady purge (1–2 scfm, 0.5 to 1 l/s) of gas to sweep through the vapor space of the tank. At the same time, the valves controlling fluid flow should be set so that the maximum amount of fluid flows through the expansion tank.
5. Increase the fluid temperature to 250°F (120°C) as measured at the heater outlet. The rate of increase should be held to 100°F (40°C) per hour or the maximum recommended for the various pieces of equipment in the system, whichever is lower. This will allow the equipment to be brought up to temperature safely and enable start-up personnel to check for leaks and ensure that all instrumentation is operating properly. Maintain the 250°F (120°C) temperature until the amount of steam or solvent vapors exiting the vent line from the expansion tank has subsided. This may require several hours.

It is essential that sufficient flow of fluid be maintained through the expansion tank during these steps so that the temperature in the tank is high enough to boil out any residual moisture or solvents from the system.

6. Set the nitrogen supply regulator and the back pressure regulator to their design set points. No further venting will occur unless the pressure in the expansion tank exceeds the specified pressure. Any further pressure increase in the tank should only result from compression of the inert gas by the expanding fluid. Any additional inert gas should enter the tank only when the tank pressure falls below the design setpoint (e.g., as it would if the system were to be shut down).

For systems which operate primarily at low temperatures and do not have the capability of heating the fluid to the temperatures outlined above, other methods of water removal may be required. The use of molecular sieves or ion exchange resins to remove the water from the fluid may be necessary.

HEALTH AND SAFETY CONSIDERATIONS

A Material Safety Data Sheet (MSDS) for SYLTHERM XLT heat transfer fluid is available by contacting your nearest Dow sales representative, or by calling 1-800-447-4369. The MSDS contains complete health and safety information regarding the use of this product. Read and understand the MSDS before handling or other-wise using this product.

SYLTHERM XLT heat transfer fluid has been studied for acute toxicological properties under the Federal Hazardous Substance Act guidelines. As a result of the FHSA study, SYLTHERM XLT heat transfer fluid has been classified as:

- Nontoxic, with regard to acute oral ingestion or dermal absorption to quantities typically contacted during normal use
- Having minimal potential for eye or skin irritation

Additionally, studies indicate that repeated, prolonged skin contact should not result in irritation. Normal industrial handling procedures are adequate to handle this product.

Unlike many low temperature heat transfer fluids, SYLTHERM XLT fluid has minimal odor and no airborne exposure limits. However, vapors of SYLTHERM XLT heat transfer fluid released into the air at temperatures above 300°F (150°C) may cause some temporary eye and/or respiratory irritation due to the partial

oxidation of the fluid. In areas with adequate ventilation, no special breathing apparatus is required. Prolonged exposures or exposures in poorly ventilated areas with high vapor concentrations should be avoided. The predominant by-products in these vapors are low-molecular-weight dimethylsiloxanes. These cyclic and linear siloxanes are commonly used in such personal care products as cosmetics and deodorants.

Leaks or spills of SYLTHERM XLT heat transfer fluid into soil typically result in the gradual break down of the polymer to form naturally occurring materials like silica, water, and carbon dioxide.

CUSTOMER SERVICE FOR USERS OF SYLTHERM XLT HEAT TRANSFER FLUID

Fluid Analysis

The Dow Chemical Company offers an analytical service for SYLTHERM XLT heat transfer fluid. It is recommended that users send a one-pint (0.5 liter) representative sample at least annually to:

North America & Pacific

The Dow Chemical Company
Larkin Lab/Thermal Fluids
1691 North Swede Road
Midland, Michigan 48674
United States of America

Europe

Dow Benelux NV
Testing Laboratory for SYLTHERM
and DOWTHERM Fluids
Oude Maasweg 4
3197 KJ Rotterdam – Botlek
The Netherlands

Latin America

Dow Quimica S.A.
Fluid Analysis Service
1671, Alexandre Dumas
Santo Amaro – Sao Paulo –
Brazil 04717-903

This analysis gives a profile of fluid changes to help identify trouble from product contamination or thermal decomposition.

When a sample is taken from a hot system it should be cooled to below 100°F (40°C) before it is put into the shipping container. Cooling the sample below 100°F (40°C) will prevent the possibility of thermal burns to personnel; also, the fluid is then below its flash point. In addition, any low boilers will not flash and be lost from the sample. Cooling can be done by either a batch or continuous process. The batch method consists of isolating the hot sample of fluid from the system in a properly designed sample collector and then cooling it to below 100°F (40°C). After it is cooled, it can be withdrawn from the sampling collector into a container for shipment.

The continuous method consists of controlling the fluid at a very low rate through a steel or stainless steel cooling coil so as to maintain it at 100°F (40°C) or lower as it comes out of the end of the cooler into the sample collector. Before a sample is taken, the sampler should be thoroughly flushed. This initial fluid should be returned to the system or disposed of in a safe manner in compliance with all laws and regulations.

It is important that samples sent for analysis be representative of the charge in the unit. Ordinarily, samples should be taken from the main circulating line of a liquid system. Occasionally, additional samples may have to be taken from other parts of the system where specific problems exist. A detailed method for analyzing the fluid to determine its quality is available upon request.

Used heat transfer fluid which has been stored in drums or tanks should be sampled in such a fashion as to ensure a representative sample.

Retrofill

SYLTHERM XLT heat transfer fluid has successfully replaced organic fluids in existing heat transfer systems. However, there are engineering considerations that should be addressed due to the unique characteristics of SYLTHERM XLT heat transfer fluid. It is suggested that The Dow Chemical Company be consulted in advance of fluid purchase and installation to discuss how best to optimize fluid performance in your system.

Storage and Shelf-life

SYLTHERM XLT heat transfer fluid, when stored in its original container, will meet sales specification requirements for a period of 5 years from date of shipment.

Store fluid at ambient temperature.

NOTE: If outside storage of drums is planned, it is suggested that some type of removable drum cover be used to prevent water from entering the drum through the bung seal.

Packaging

SYLTHERM XLT heat transfer fluid is supplied in 35-lb (16-kg) containers (net weight) in the U.S. only, and in 375-lb (170-kg) containers (net weight) globally, as well as in bulk quantities.

Table 1 — Physical Properties of SYLTHERM XLT Heat Transfer Fluid¹

Composition:	Dimethyl Polysiloxane	
Color:	Crystal Clear Liquid	
<u>Property</u>	<u>English Units</u>	<u>SI Units</u>
Viscosity 1.4 cP @ 77°F 1.4 mPa·s @ 25°C
Flash Point ² , Closed Cup 116°F 47°C
Flash Point ³ , Open Cup 130°F 54°C
Autoignition Temperature, ASTM D-2155 662°F 350°C
Acid Number, Typical 0.01	
Freeze Point -168°F -111°C
Density @ 77°F (25°C) 7.1 lb/gal 852 kg/m ³
Specific Gravity @ 77°F (25°C) 0.85	
Heat of Combustion 14,100 Btu/lb 32,800 kJ/kg
Average Molecular Weight 317	
Estimated Critical Constants		
T _c 620°F 327°C
P _c 12 atm 12.16 bar
V _c 0.063 ft ³ /lb 3.9 l/kg

¹Not to be construed as specifications.

²ASTM D92

³ASTM D93

Table 2 — Select Saturated Vapor Properties of SYLTHERM XLT Fluid (English Units) Values are estimated

Temp. °F	ΔH_{lv} Btu/lb	Z_{vapor}	C_p/C_v	Vapor Molecular Weight
100	106.7	0.9991	1.027	230.1
120	103.7	0.9985	1.026	232.8
140	100.8	0.9976	1.025	235.3
160	98.1	0.9963	1.024	237.7
180	95.4	0.9945	1.024	240.1
200	92.7	0.9921	1.023	242.3
220	90.1	0.9889	1.023	244.6
240	87.6	0.9849	1.023	246.7
260	85.0	0.9798	1.023	248.9
280	82.5	0.9736	1.023	251.1
300	79.9	0.9661	1.023	253.2
320	77.3	0.9572	1.023	255.4
340	74.7	0.9468	1.024	257.6
360	72.0	0.9348	1.025	259.9
380	69.2	0.9210	1.026	262.2
400	66.4	0.9054	1.028	264.6
420	63.4	0.8877	1.030	267.1
440	60.3	0.8678	1.032	269.7
460	57.1	0.8457	1.036	272.4
480	53.7	0.8210	1.041	275.4
500	50.1	0.7935	1.047	278.5
520	46.2	0.7629	1.056	282.0
540	41.9	0.7286	1.069	285.8
560	37.3	0.6901	1.089	290.1
580	32.1	0.6461	1.121	295.1
600	26.1	0.5946	1.181	301.1

Table 3 — Select Saturated Vapor Properties of SYLTHERM XLT Fluid (SI Units) Values are estimated

Temp. °C	ΔH_{lv} kJ/kg	Z_{vapor}	C_p/C_v	Vapor Molecular Weight
45	243.7	0.9987	1.026	231.8
55	237.5	0.9981	1.026	234.2
65	231.6	0.9971	1.025	236.4
75	225.9	0.9957	1.024	238.6
85	220.3	0.9940	1.024	240.7
95	214.8	0.9917	1.023	242.7
105	209.3	0.9887	1.023	244.7
115	204.0	0.9851	1.023	246.6
125	198.6	0.9806	1.023	248.6
135	193.3	0.9753	1.023	250.5
145	187.9	0.9689	1.023	252.5
155	182.5	0.9614	1.023	254.4
165	177.1	0.9528	1.023	256.4
175	171.5	0.9428	1.024	258.4
185	165.8	0.9315	1.025	260.4
195	160.0	0.9188	1.026	262.5
205	154.0	0.9045	1.028	264.7
215	147.8	0.8886	1.030	266.9
225	141.4	0.8710	1.032	269.3
235	134.7	0.8514	1.035	271.7
245	127.7	0.8299	1.039	274.3
255	120.3	0.8062	1.044	277.1
265	112.4	0.7801	1.051	280.0
275	104.0	0.7513	1.060	283.2
285	95.0	0.7194	1.073	286.8
295	85.1	0.6839	1.093	290.8
305	74.1	0.6438	1.123	295.3
315	61.5	0.5975	1.176	300.8

Table 4 — Saturated Liquid Properties of SYLTHERM XLT Fluid (English Units)

Temp. °F	Specific Heat Btu/lb°F	Density lb/ft ³	Therm. Cond. Btu/hr ft ² (°F/ft)	Viscosity cps	Vapor Pressure psia
-150	0.363	61.23	0.0776	90.2	
-130	0.368	60.52	0.0765	33.7	
-110	0.374	59.80	0.0753	19.0	
-90	0.379	59.09	0.0742	12.3	
-70	0.385	58.38	0.0730	8.4	
-50	0.391	57.66	0.0717	6.0	
-30	0.396	56.95	0.0705	4.5	
-10	0.402	56.24	0.0692	3.4	
10	0.407	55.52	0.0679	2.6	
30	0.413	54.81	0.0666	2.1	
50	0.418	54.10	0.0652	1.7	
70	0.424	53.38	0.0639	1.4	
90	0.430	52.67	0.0625	1.2	
110	0.435	51.96	0.0610	0.99	0.1
130	0.441	51.24	0.0596	0.85	0.2
150	0.446	50.53	0.0581	0.74	0.3
170	0.452	49.82	0.0567	0.65	0.6
190	0.458	49.10	0.0551	0.58	0.9
210	0.463	48.39	0.0536	0.52	1.5
230	0.469	47.68	0.0521	0.47	2.2
250	0.474	46.96	0.0505	0.42	3.2
270	0.480	46.25	0.0489	0.39	4.6
290	0.485	45.54	0.0473	0.35	6.4
310	0.491	44.82	0.0457	0.33	8.7
330	0.497	44.11	0.0441	0.30	11.6
350	0.502	43.40	0.0424	0.28	15.2
370	0.508	42.68	0.0407	0.26	19.6
390	0.513	41.97	0.0390	0.25	25.0
410	0.519	41.26	0.0373	0.23	31.3
430	0.524	40.54	0.0356	0.22	38.8
450	0.530	39.83	0.0339	0.21	47.5
470	0.536	39.12	0.0321	0.20	57.6
490	0.541	38.40	0.0304	0.19	69.1
510	0.547	37.69	0.0286	0.18	82.2
530	0.552	36.98	0.0268	0.17	97.0
550	0.558	36.26	0.0250	0.16	113.6

Table 5 — Saturated Liquid Properties of SYL THERM XLT Fluid (SI Units)

Temp. °C	Specific Heat kJ/kg K	Density kg/m ³	Therm. Cond. W/m K	Viscosity mPa•s	Vapor Pressure kPa
-100	1.520	978.5	0.1341	78.6	
-90	1.541	968.3	0.1324	33.7	
-80	1.562	958.0	0.1306	20.0	
-70	1.583	947.7	0.1288	13.3	
-60	1.604	937.4	0.1269	9.4	
-50	1.625	927.2	0.1251	6.9	
-40	1.646	916.9	0.1231	5.2	
-30	1.66	906.67	0.1212	4.0	
-20	1.688	896.4	0.1192	3.1	
-10	1.709	886.1	0.1171	2.5	
0	1.730	875.8	0.1150	2.0	
10	1.751	865.5	0.1129	1.7	
20	1.772	855.3	0.1108	1.4	0.2
30	1.793	845.0	0.1086	1.2	0.3
40	1.814	834.7	0.1064	1.0	0.6
50	1.835	824.5	0.1042	0.91	1.1
60	1.856	814.2	0.1019	0.80	1.8
70	1.877	803.9	0.0996	0.70	3.0
80	1.898	793.6	0.0973	0.63	4.7
90	1.919	783.4	0.0949	0.57	7.2
100	1.940	773.1	0.0925	0.51	10.6
110	1.961	762.8	0.0901	0.47	15.3
120	1.982	752.6	0.0877	0.43	21.5
130	2.003	742.3	0.0852	0.39	29.7
140	2.024	732.0	0.0827	0.36	40.1
150	2.045	721.7	0.0802	0.34	53.2
160	2.066	711.5	0.0777	0.31	69.5
170	2.087	701.2	0.0751	0.29	89.4
180	2.108	690.9	0.0725	0.28	113.5
190	2.129	680.7	0.0699	0.26	142.2
200	2.150	670.4	0.0673	0.24	176.2
210	2.171	660.1	0.0646	0.23	215.9
220	2.192	649.8	0.0620	0.22	261.9
230	2.213	639.6	0.0593	0.21	314.8
240	2.234	629.3	0.0566	0.20	375.1
250	2.255	619.0	0.0538	0.19	443.4
260	2.276	608.8	0.0511	0.18	520.3
270	2.297	598.5	0.0483	0.17	606.2
280	2.318	588.2	0.0455	0.17	701.8
290	2.339	577.9	0.0427	0.16	807.4

Figure 3 — Thermal Conductivity of SYLTHERM XLT Fluid (English Units)

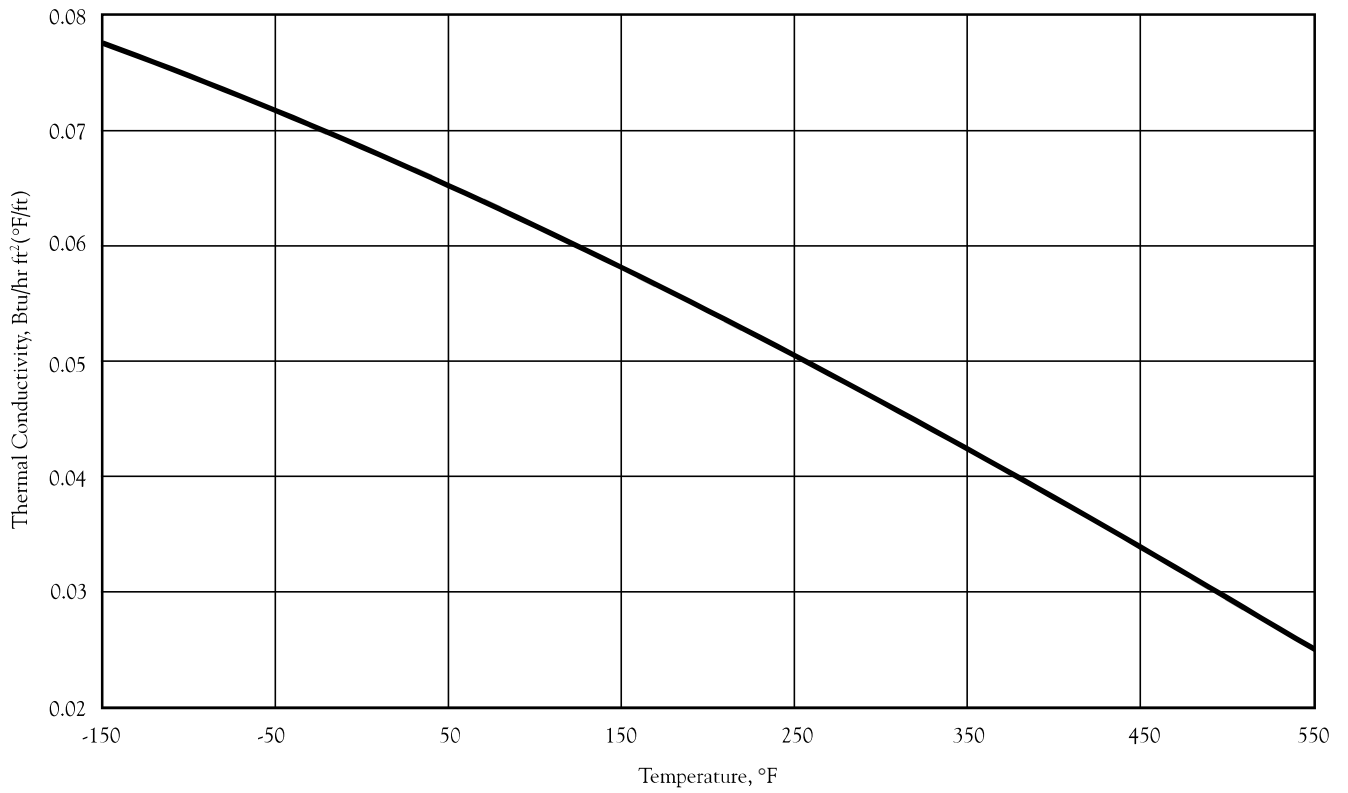


Figure 4 — Thermal Conductivity of SYLTHERM XLT Fluid (SI Units)

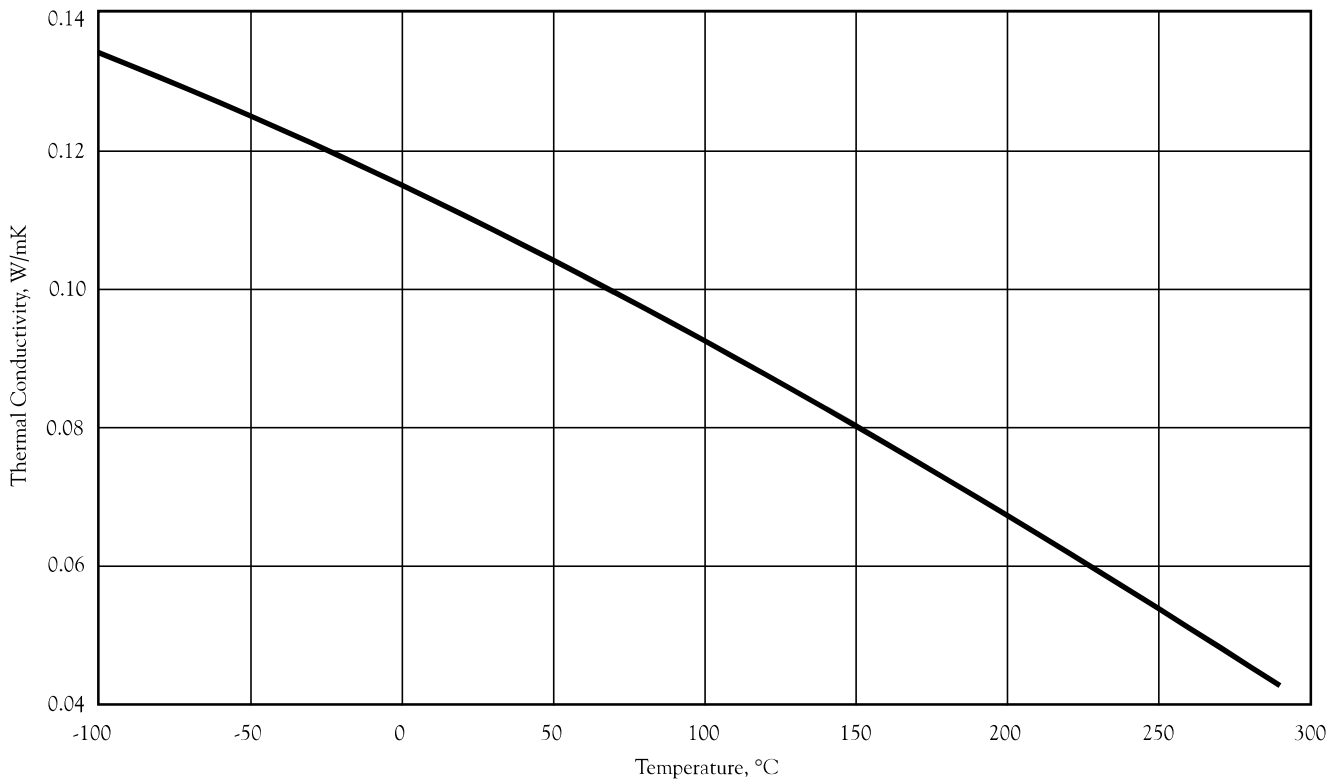


Figure 5 — Heat of Vaporization of SYLTHERM XLT Fluid (English Units)

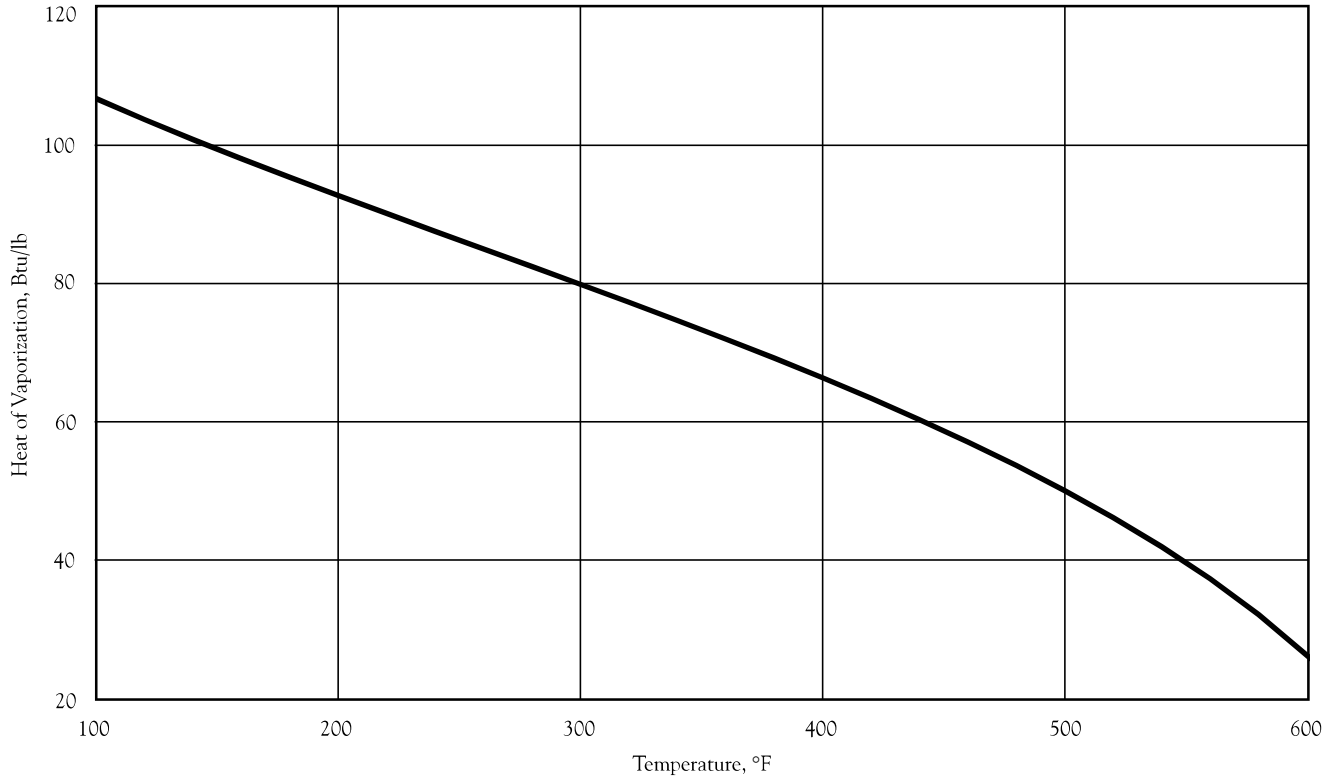


Figure 6 — Heat of Vaporization of SYLTHERM XLT Fluid (SI Units)

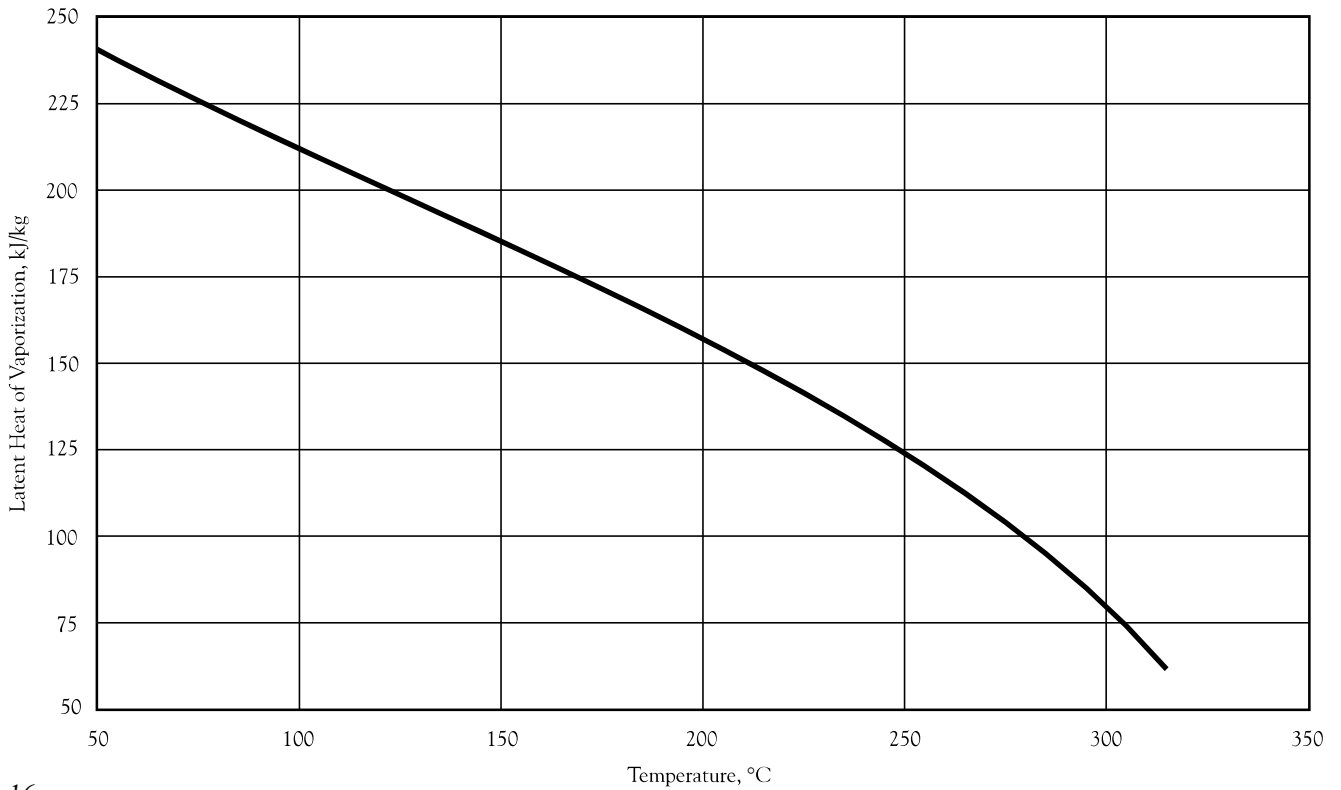


Figure 7 — Vapor Pressure of SYLTHERM XLT Fluid (English Units)

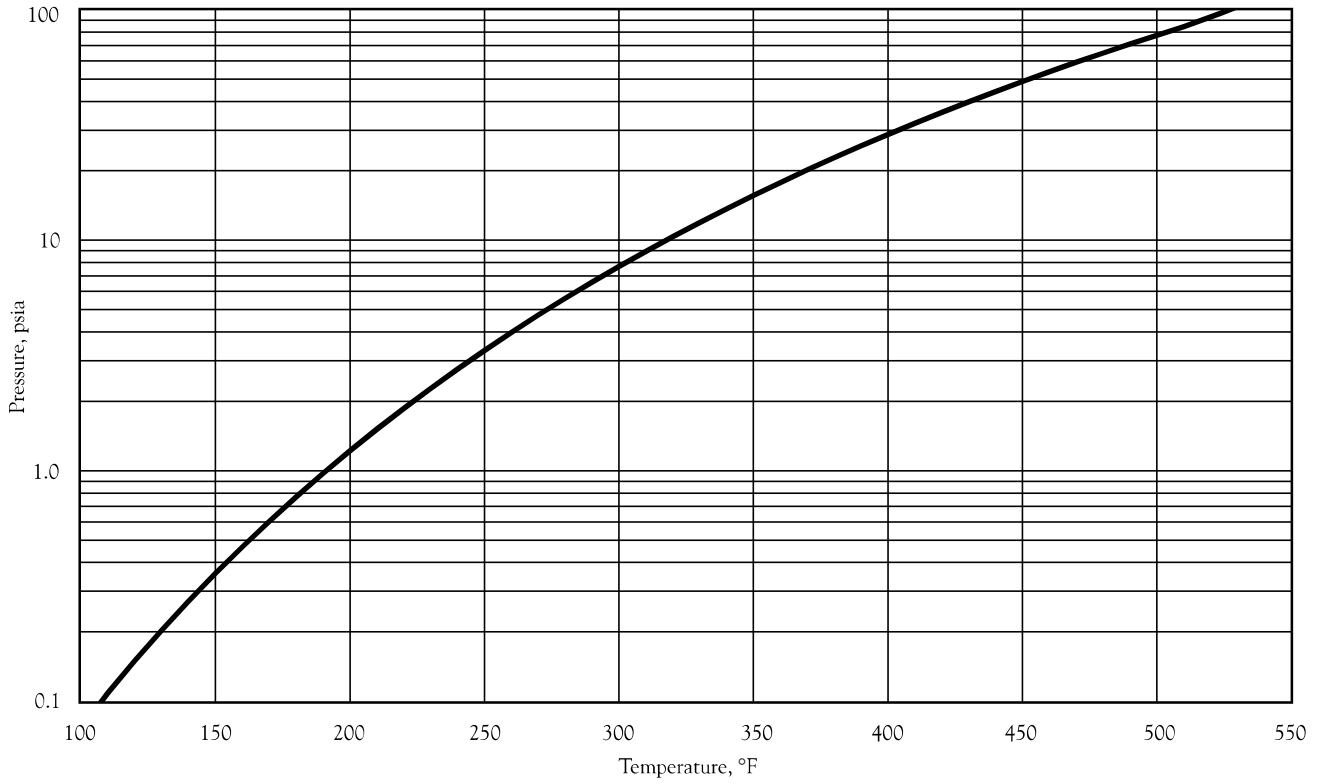


Figure 8 — Vapor Pressure of SYLTHERM XLT Fluid (SI Units)

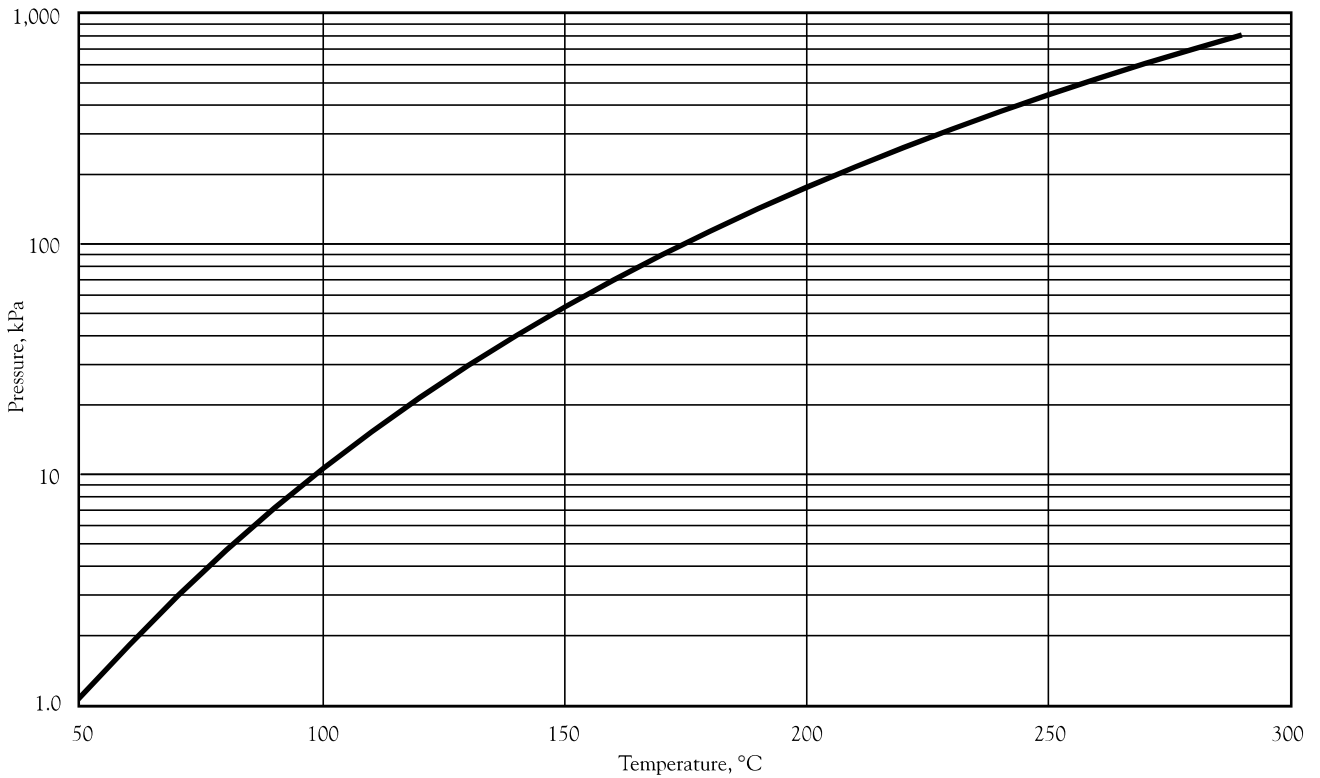


Figure 9 — Specific Heat of SYLTHERM XLT Fluid (English Units)

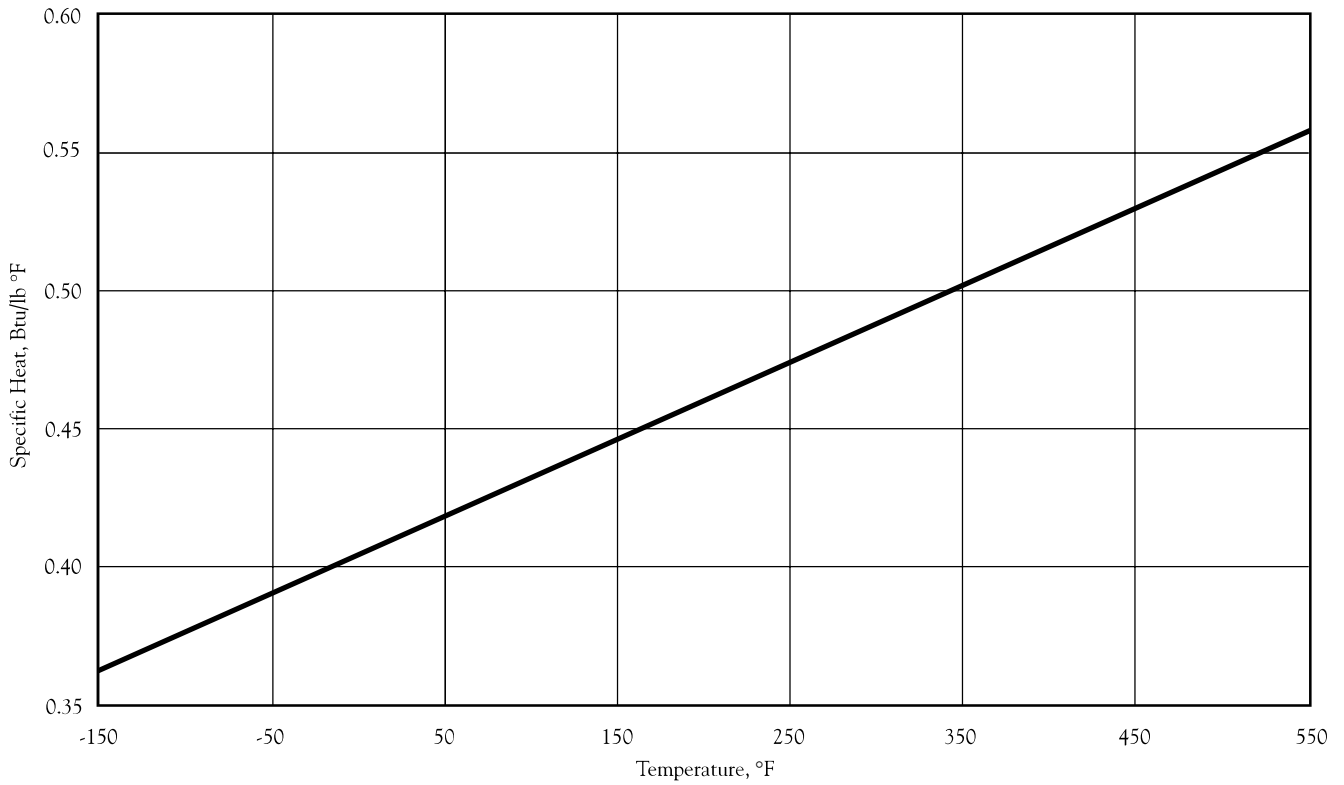


Figure 10 — Specific Heat of SYLTHERM XLT Fluid (SI Units)

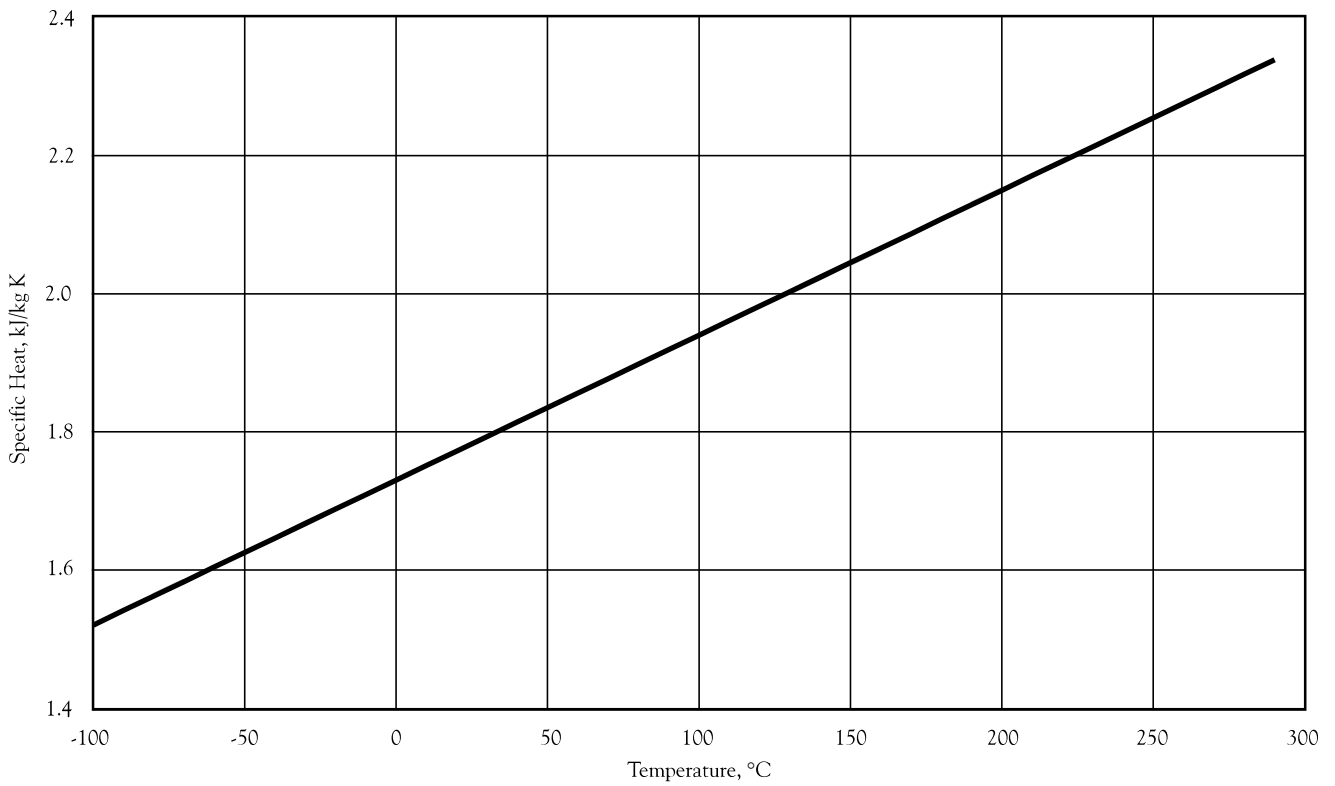


Figure 11 — Density of SYLTHERM XLT Fluid (English Units)

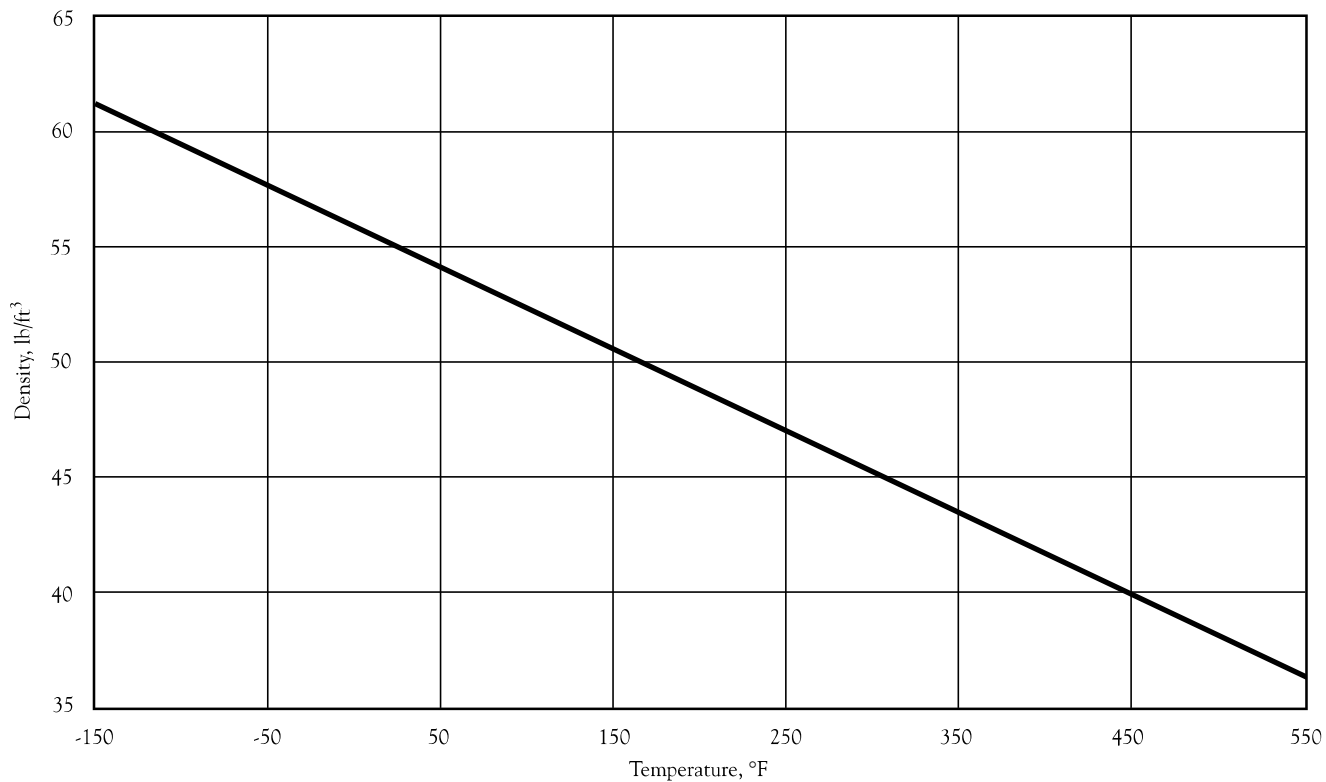


Figure 12 — Density of SYLTHERM XLT Fluid (SI Units)

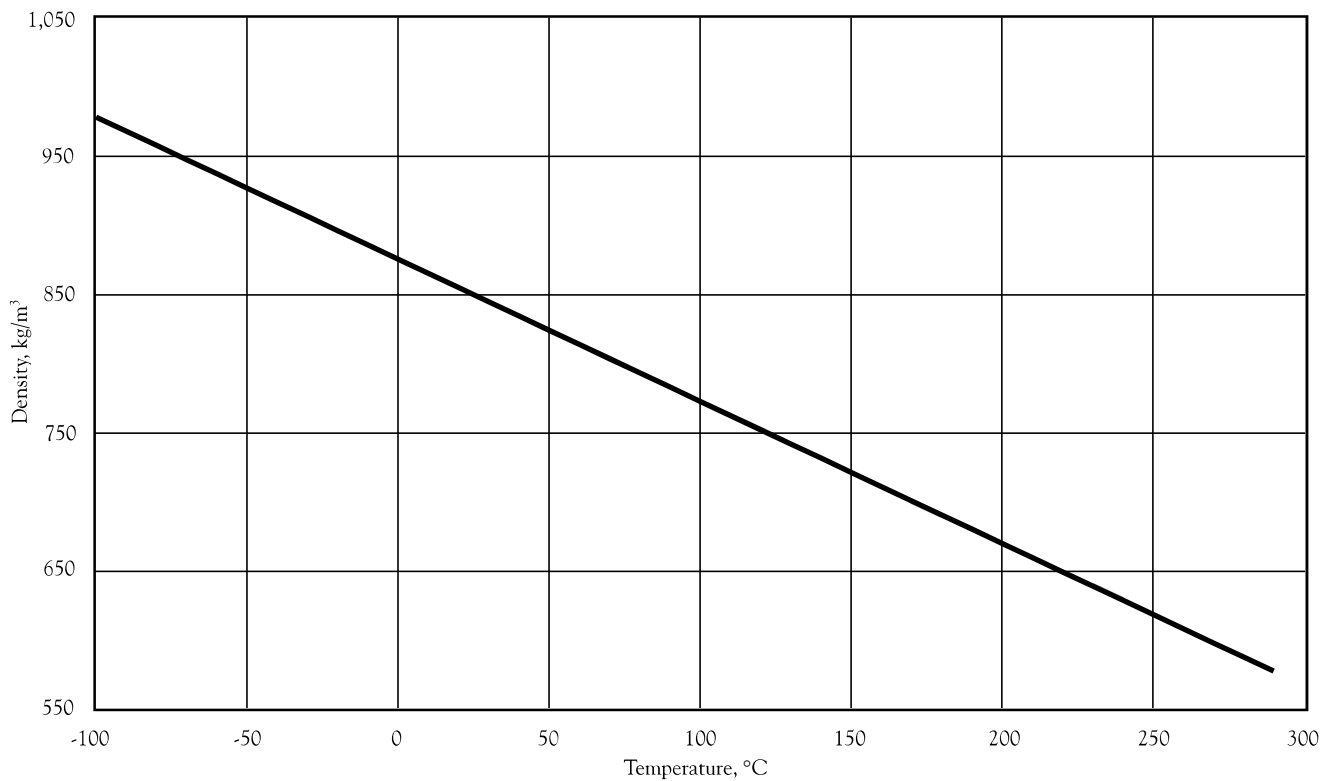


Figure 13 — Viscosity of SYLTHERM XLT Fluid (English Units)

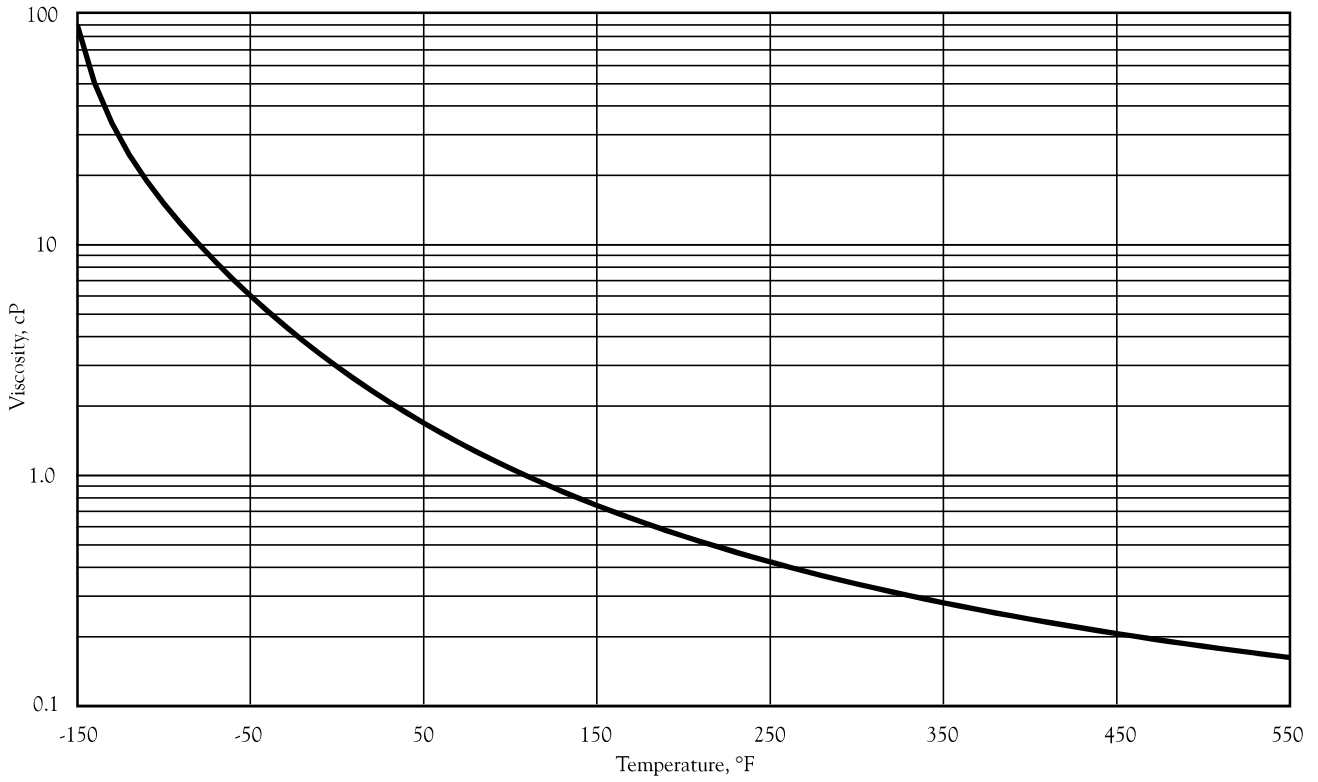


Figure 14 — Viscosity of SYLTHERM XLT Fluid (SI Units)

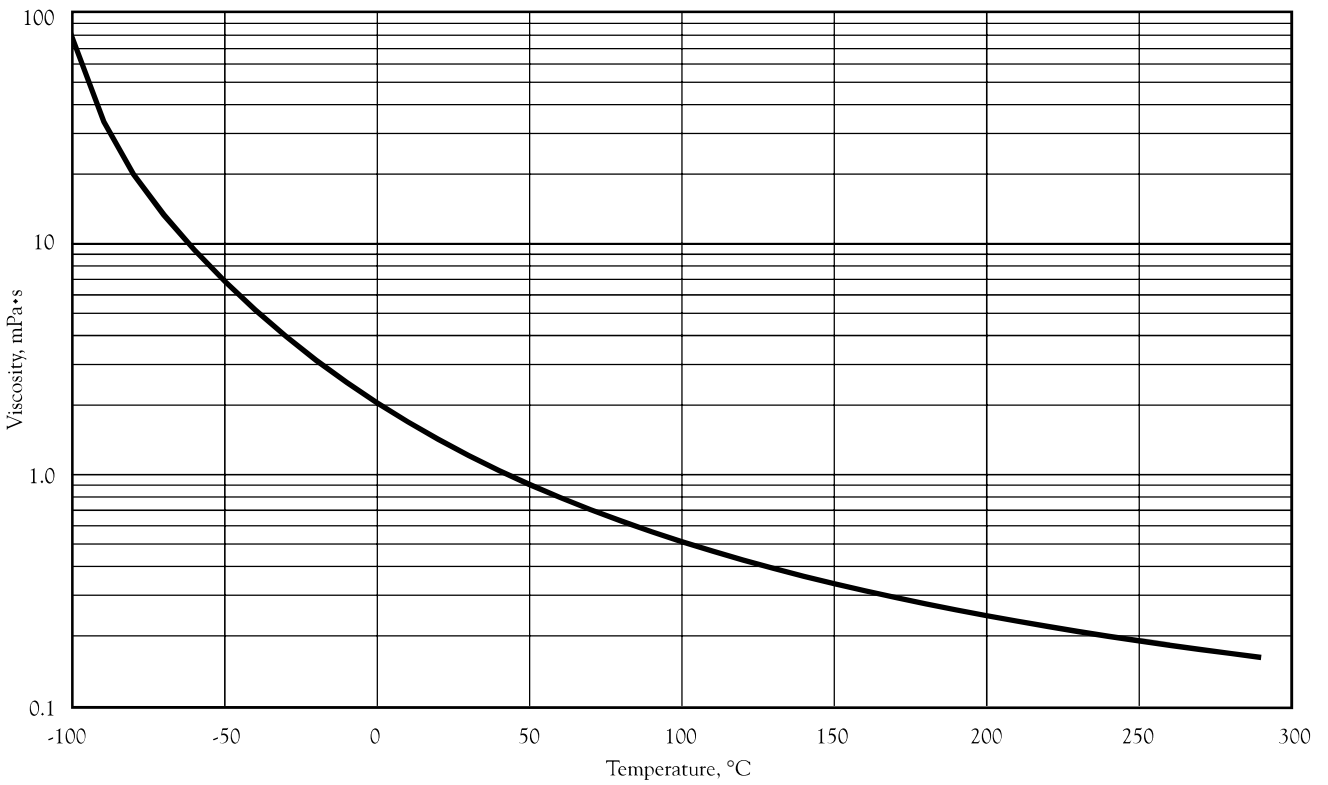


Figure 15 — Solubility of Water in SYLTHERM XLT Fluid (English Units)

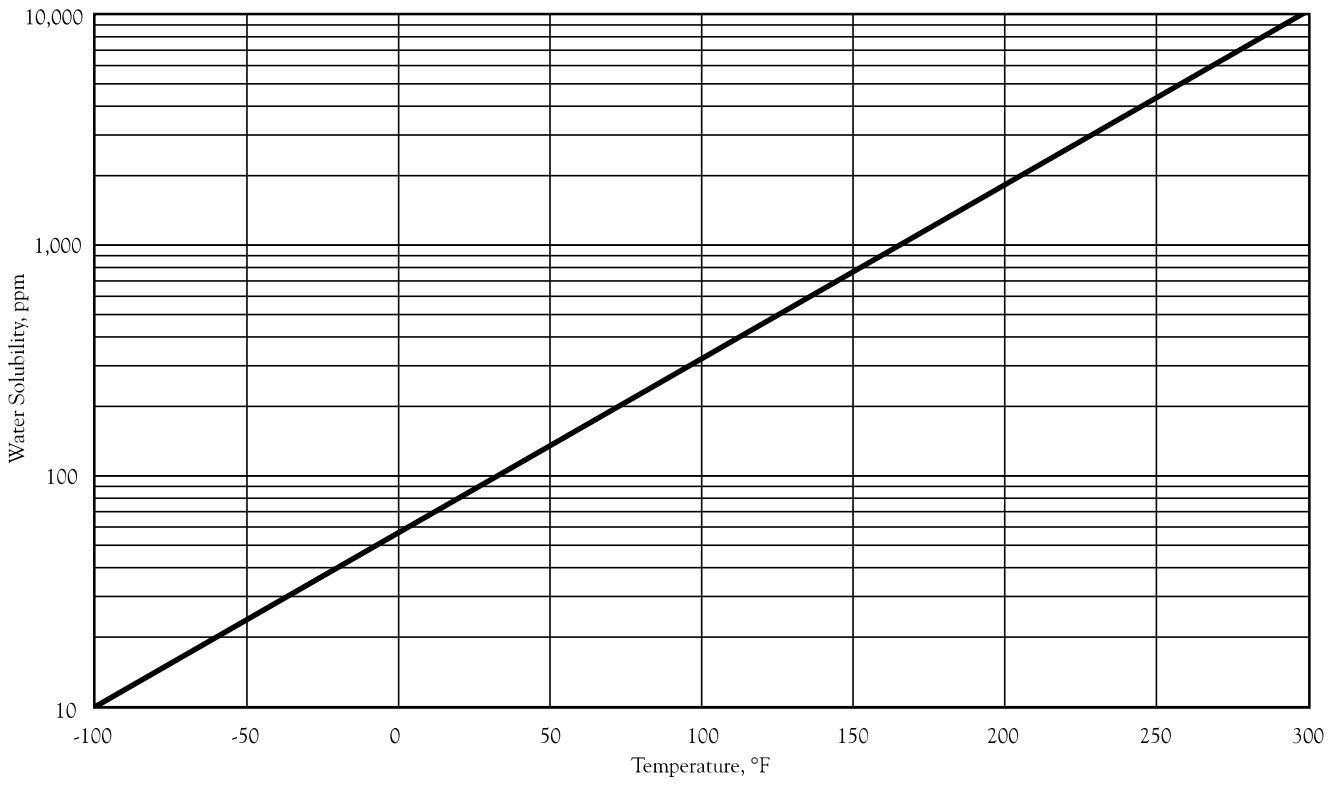


Figure 16 — Solubility of Water in SYLTHERM XLT Fluid (SI Units)

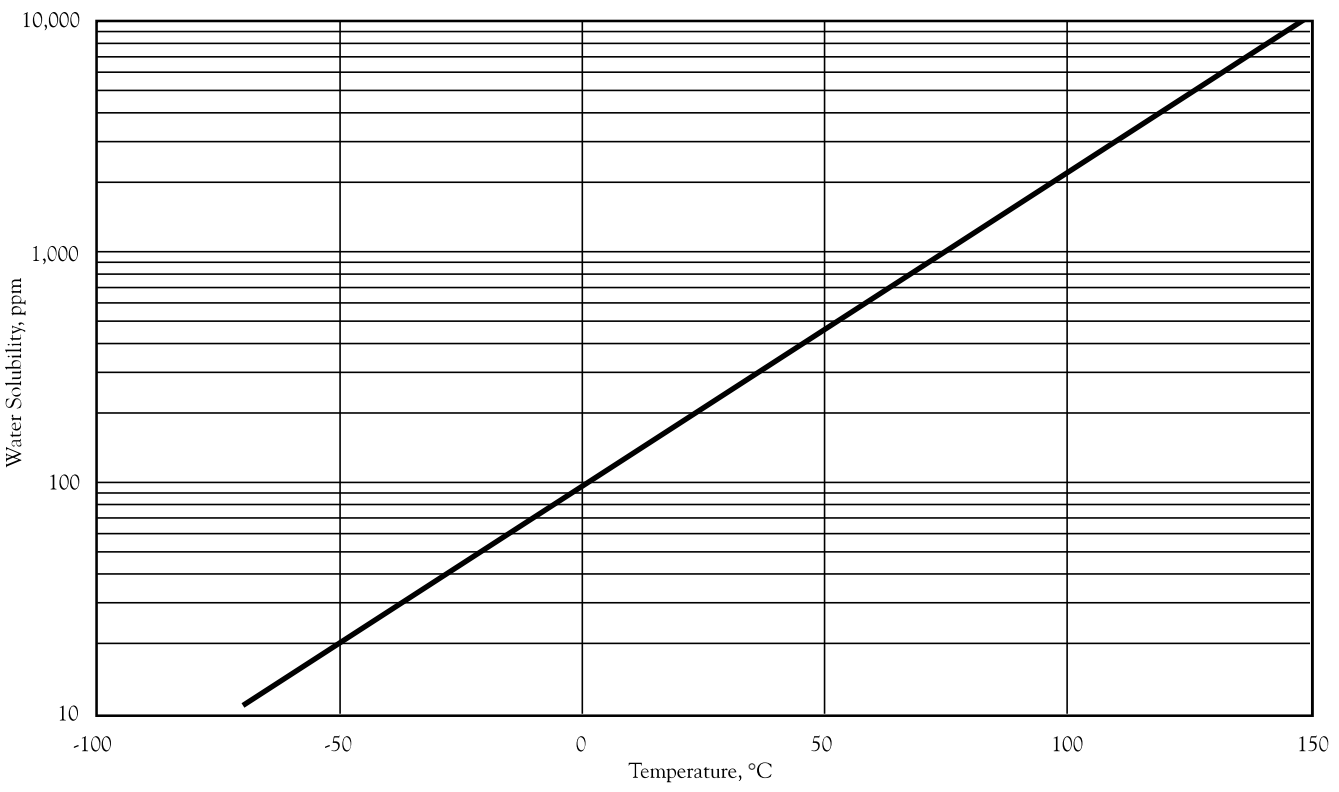
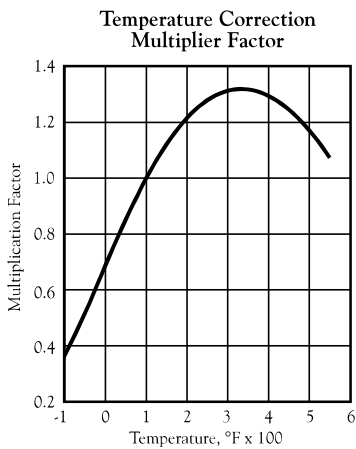
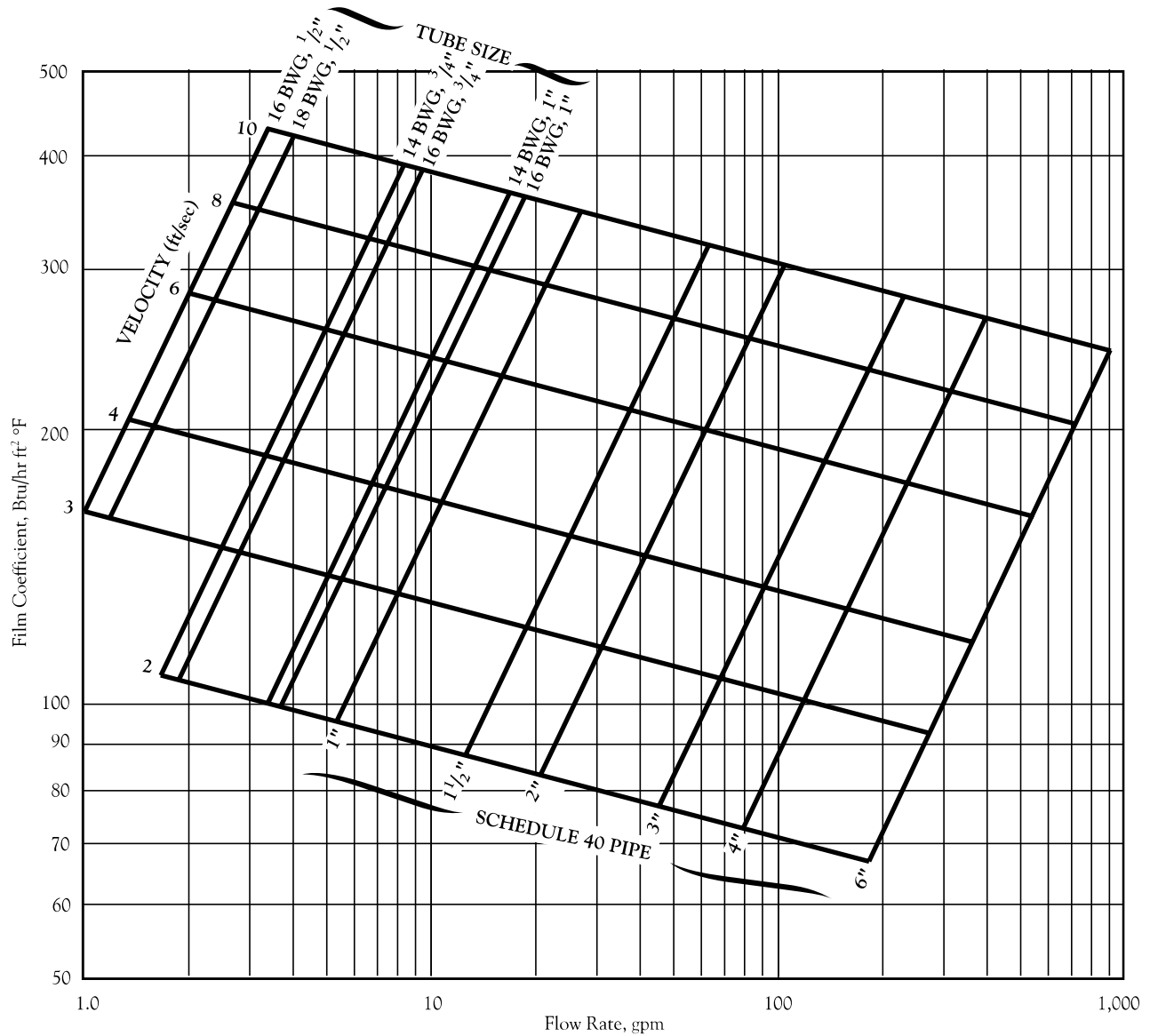


Figure 17 — Liquid Film Coefficient for SYLTHERM XLT Fluid Inside Pipes and Tubes (Turbulent Flow Only) (English Units)



Sieder and Tate equation
Process Heat Transfer,
D.Q. Kern (1950) p.103

$$Nu = 0.027Re^{0.8}Pr^{1/3} \left(\frac{\mu}{\mu_w}\right)^{0.14}$$

Chart based on $\left(\frac{\mu}{\mu_w}\right)^{0.14} = 1$

Note: The values in this graph are based on the viscosity of fluid as supplied.

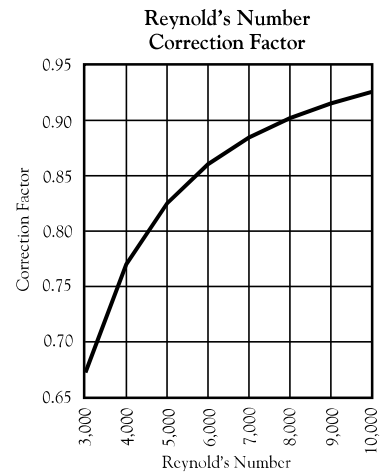
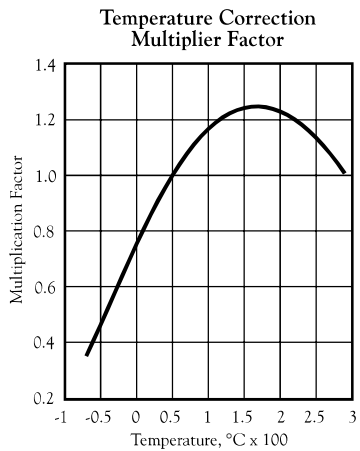
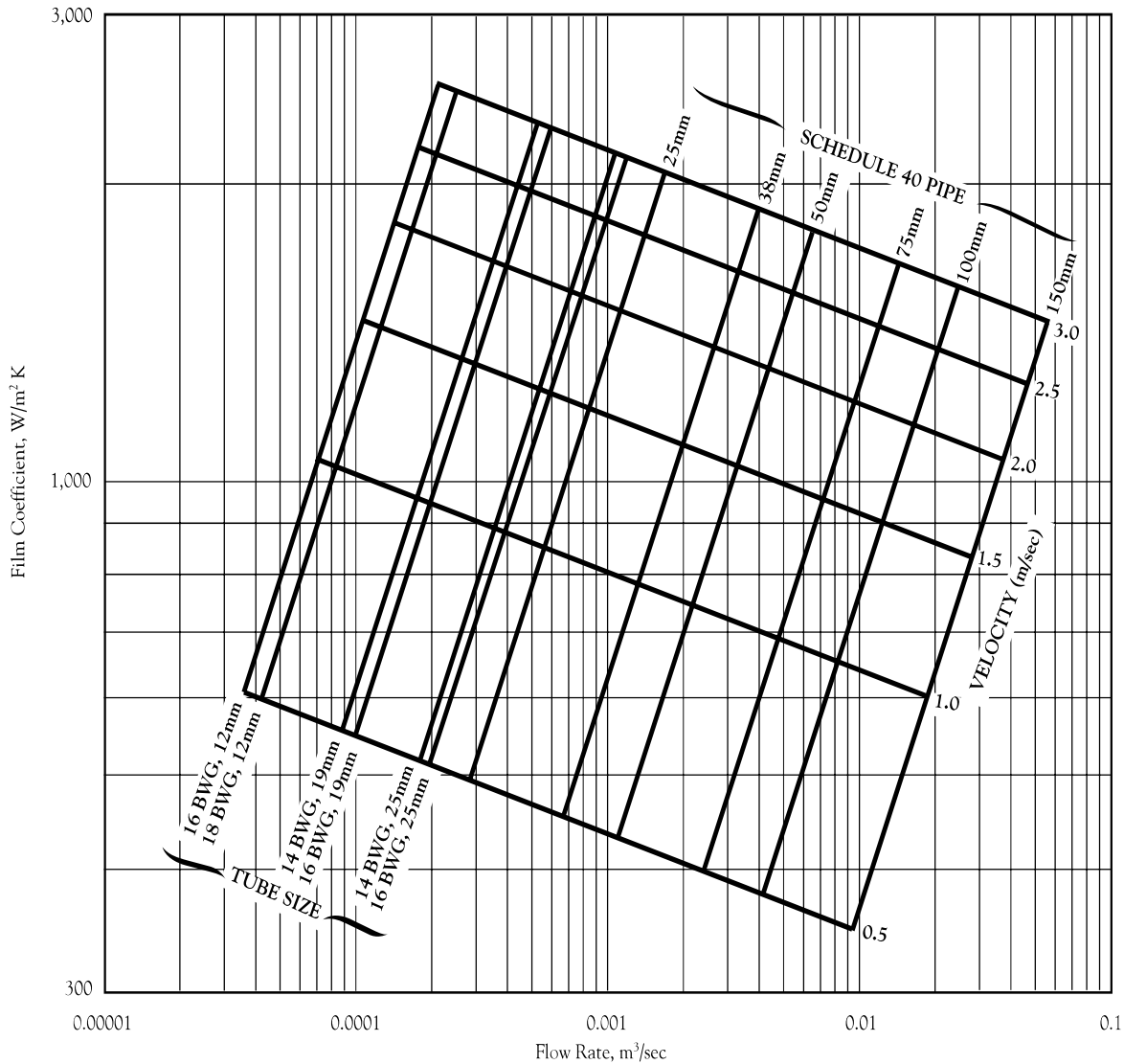


Figure 18 — Liquid Film Coefficient for SYLTHERM XLT Fluid Inside Pipes and Tubes (Turbulent Flow Only) (SI Units)



Sieder and Tate equation
Process Heat Transfer,
D.Q. Kern (1950) p.103

$$Nu = 0.027Re^{0.8}Pr^{1/3} \left(\frac{\mu}{\mu_w} \right)^{0.14}$$

Chart based on $\left(\frac{\mu}{\mu_w} \right)^{0.14} = 1$

Note: The values in this graph are based on the viscosity of fluid as supplied.

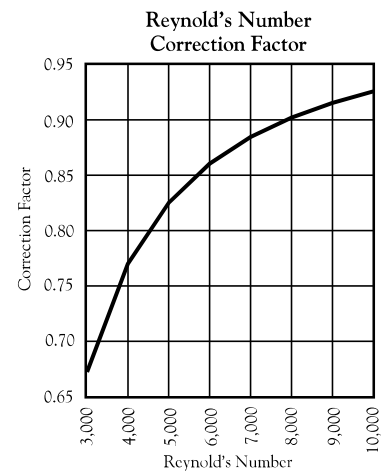


Figure 19 — Pressure Drop vs. Flow Rate for SYLTHERM XLT Fluid in Schedule 40 Nominal Pipe and BWG Tube (English Units)

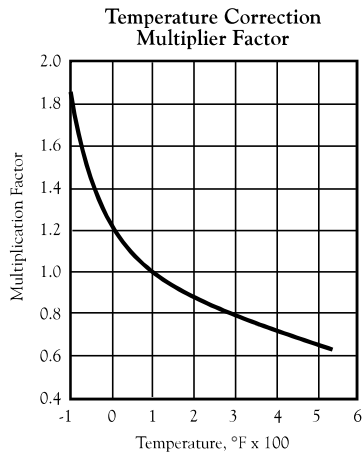
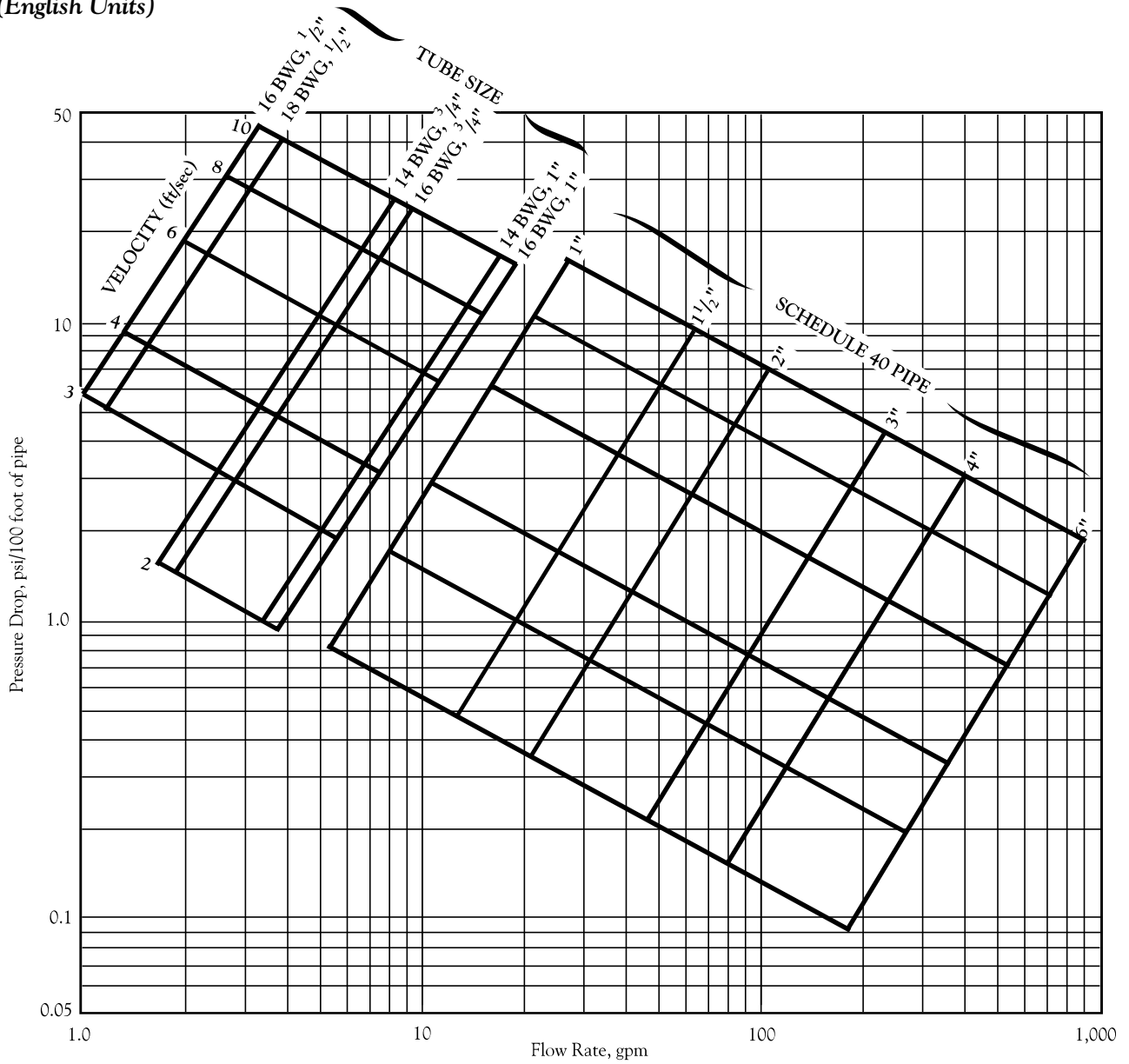


Figure 20 — Pressure Drop vs. Flow Rate for SYLTHERM XLT Fluid in Schedule 40 Nominal Pipe and BWG Tube (SI Units)

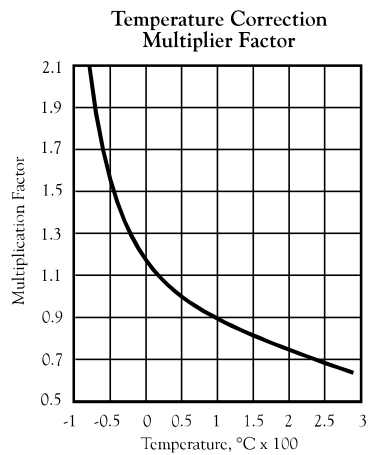
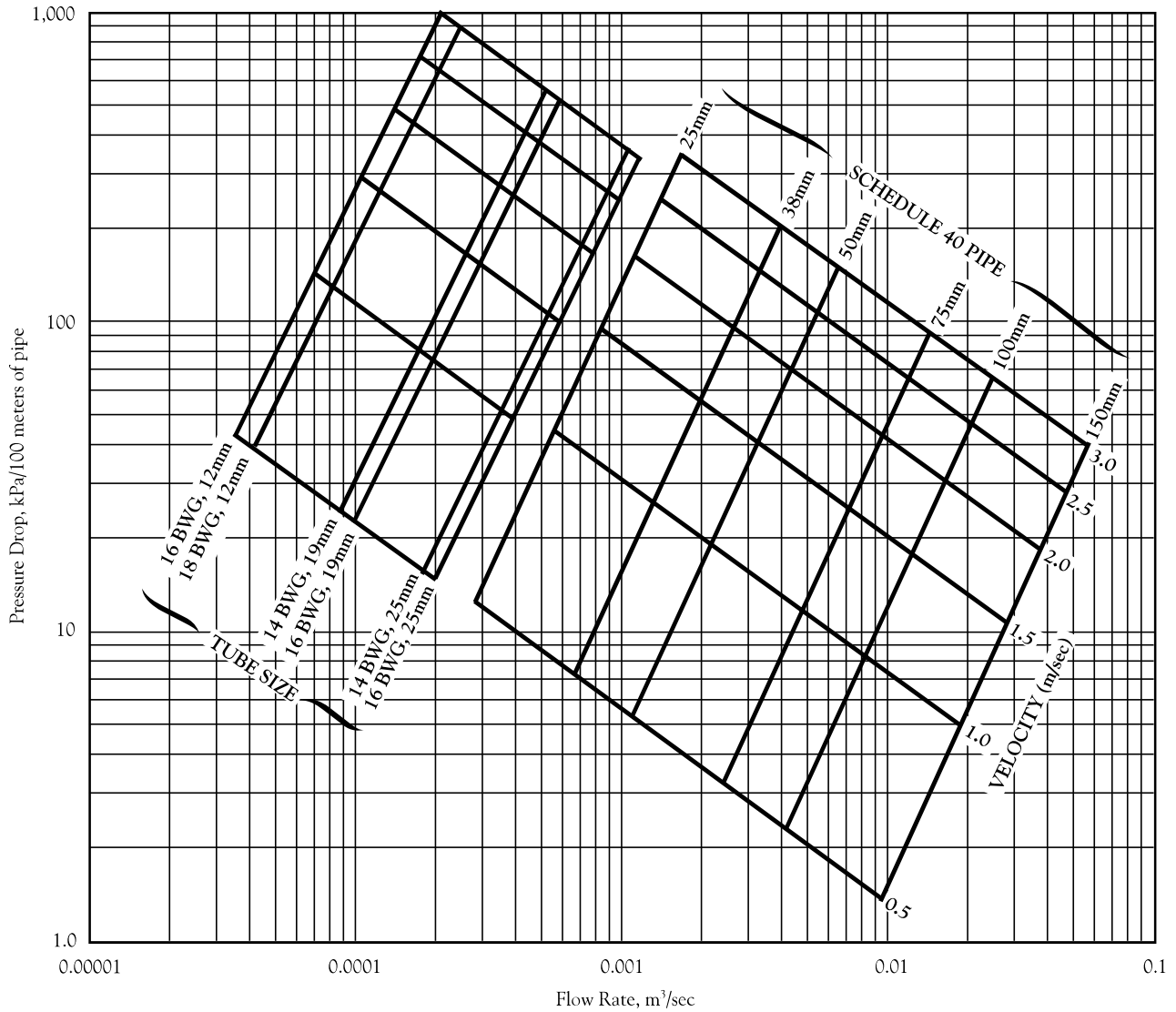


Figure 21 — Thermal Expansion of Liquid SYLTHERM XLT Fluid (English Units)

Basis: 1 gallon @75°F

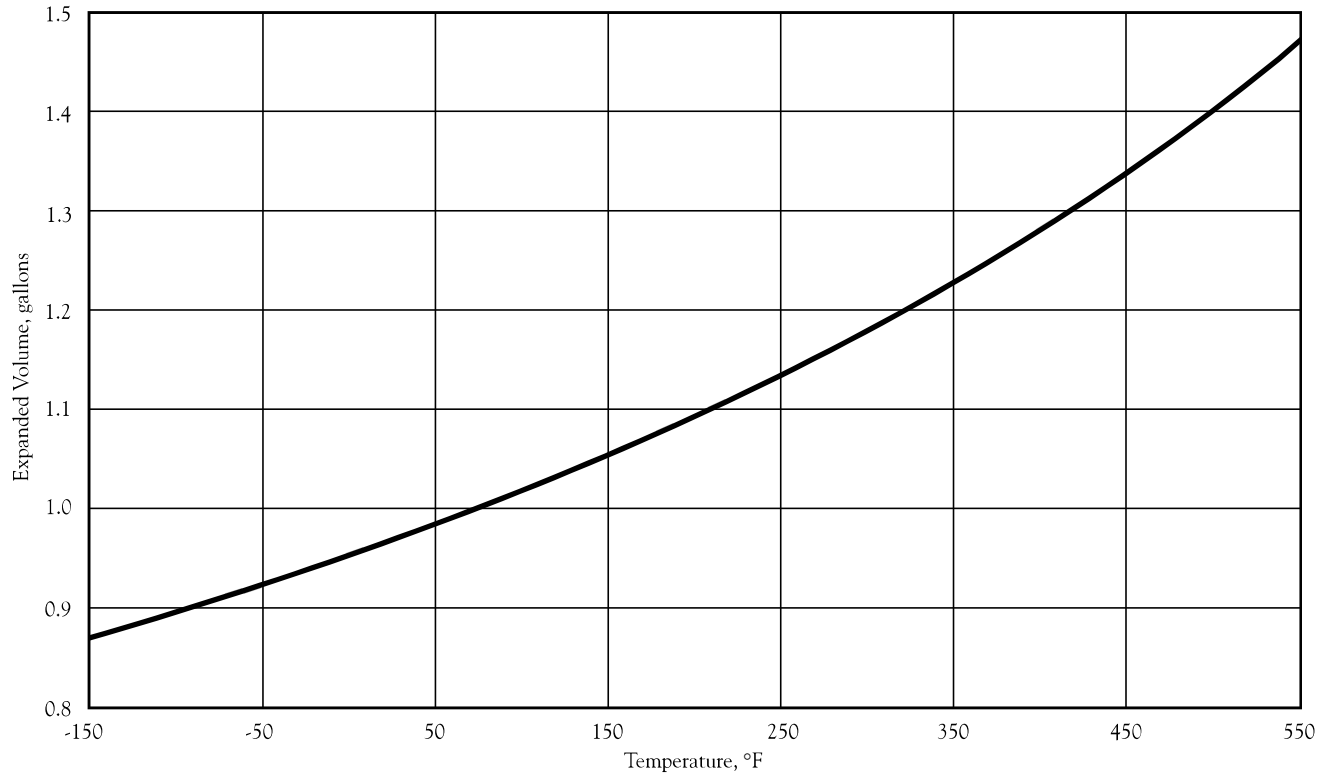
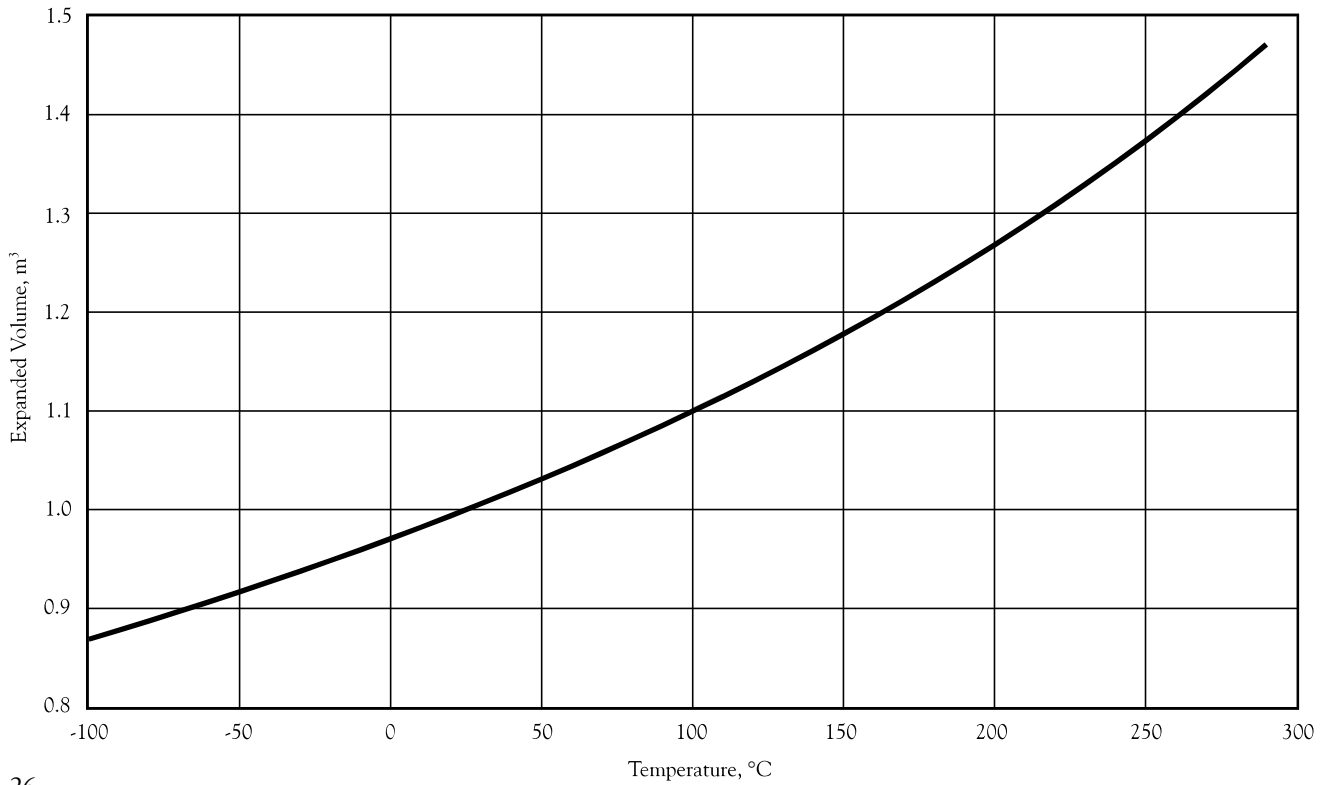


Figure 22 — Thermal Expansion of Liquid SYLTHERM XLT Fluid (SI Units)

Basis: 1 m³ @25°C

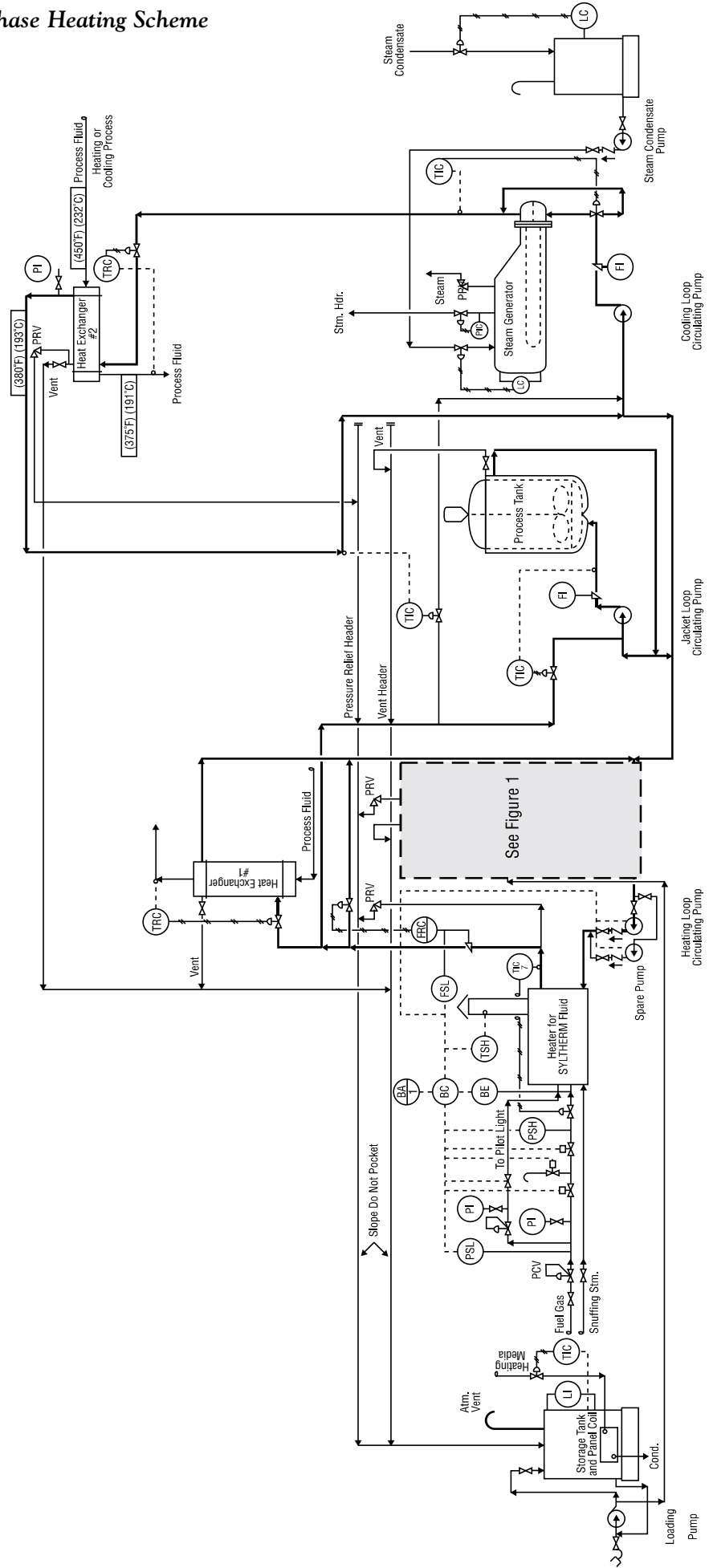


**Figure 23 — Typical Liquid Phase Heating Scheme
Using SYLATHERM Fluids**

Instrument Legend

- BA — Burner Alarm
- BC — Burner Control
- BE — Burner Element (Fire-Eye)
- FI — Flow Indicator (Orifice)
- FRC — Flow Recording Controller
- FSL — Flow Switch Low
- LC — Level Controller
- PVC — Pressure Control Valve
- PI — Pressure Indicator
- PIC — Pressure Indicating Controller
- PRV — Pressure Relief Valve
- PSH — Pressure Switch High
- PSL — Pressure Switch Low
- TIC — Temperature Indicating Controller
- TRC — Temperature Recorder Controller
- TSH — Temperature Switch High

- Principal Circuits with SYLATHERM Fluid
- Electrical Lines
- - - - Instrument Air Lines



SYLTHERM XLT Heat Transfer Fluid

Product Technical Data

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In The Pacific: +886 22 547 8731 • FAX: +886 22 713 0092

In Other Global Areas: 1-517-832-1556 • FAX: 1-517-832-1465

<http://www.dow.com/heattrans>

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